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Summary

Brush seals are compliant contacting seals and have significantly lower leakage than labyrinth seals in gas turbine applications. Their long life and low leakage make them candidates for use in rocket engine turbopumps. Brush seals, 50.8 mm (2 in.) in diameter with a nominal 127-µm (0.005-in.) radial interference, were tested in liquid nitrogen (LN2) and liquid hydrogen (LH₂) at shaft speeds up to 35 000 and 65 000 rpm, respectively, and at pressure drops up to 1.21 MPa (175 psid) per brush. A labyrinth seal was also tested in liquid nitrogen to provide a baseline. The LN₂ leakage rate of a single brush seal with an initial radial shaft interference of 127 µm (0.005 in.) measured one-half to one-third the leakage rate of a 12-tooth labyrinth seal with a radial clearance of 127 µm (0.005 in.). Two brushes spaced 7.21 µm (0.248 in.) apart leaked about one-half as much as a single brush, and two brushes tightly packed together leaked about three-fourths as much as a single brush. The maximum measured groove depth on the Inconel 718 rotor with a surface finish of 0.81 \mum (32 \muin.) was 25 \mum (0.0010-in.) after 4.3 hr of shaft rotation in liquid nitrogen. The Haynes-25 bristles were approximately 25 to 76 µm (0.001 to 0.003 in.) under the same conditions. Wear results in liquid hydrogen were significantly different. In liquid hydrogen the rotor did not wear, but the bristle material transferred onto the rotor and the initial 127-µm (0.005-in.) radial interference was consumed. Relatively high leakage rates were measured in liquid hydrogen. More testing is required to verify the leakage performance, to validate and calibrate analysis techniques, and to determine the wear mechanisms. Performance, staging effects, and preliminary wear results are presented.

Introduction

Brush seals are being tested in cryogenic fluids to determine their usefulness in cryogenic turbopumps for rocket engine systems. Successfully operated for thousands of hours in gas turbine applications, brush seals have shown a significant improvement in leakage performance over labyrinth seals (a 50- to 90-percent reduction initially and for long life applications, a 20- to 25-percent reduction, refs. 1 to 3). Their low leakage and long life make brush seals candidates for use in rocket engine turbopumps, particularly for space-based engines and reusable launch engines. The low leakage requirement is critical in meeting the wide-operating-range requirement of space engines in which seal leakage can significantly reduce engine performance at low thrust levels. Brush seals have also been shown to be more rotordynamically stable than labyrinth seals (ref. 4). Little brush seal data exist in the open literature and that which does has focused on gas applications (refs. 5 to 9). The first brush seal data taken in liquid nitrogen were obtained by Rocketdyne under a cooperative agreement with the NASA Lewis Research Center (ref. 10). This report will present liquid nitrogen and the first liquid hydrogen brush seal data known to be taken.

In a cryogenic turbopump, brush seals may be used to seal either liquid hydrogen or liquid oxygen at locations near the pump or the bearings, or they may be used to seal hot gaseous hydrogen, combustion gases, warm gaseous oxygen, or helium at locations near the turbine or purge seals. In this environment, large temperature gradients, oxygen compatibility, and hydrogen embrittlement are concerns. Also, shaft speeds can be quite high, up to 200 000 rpm for future upperstage rocket engine liquid hydrogen turbopumps. Because brush seals are compliant contacting seals, their wear rate and wear mechanism are important. To address the full range of conditions that a brush seal may be exposed to in a cryogenic turbopump, hot gas testing is also being done at the NASA Lewis Research Center (ref. 11).

The testing of brush seals in liquid nitrogen and liquid hydrogen was conducted at the NASA Lewis Research Center at shaft speeds up to 35 000 and 65 000 rpm, respectively, and at pressure drops up to 1.21 (175 psid) per seal. A labyrinth seal was also tested in LN₂ to provide a baseline for comparison. The apparatus, test procedures and operating conditions, calculations, and prediction tools are described. The results of the liquid nitrogen data presented and discussed include labyrinth seal and single brush seal steady-state performance, staging effects, and preliminary wear data. The hydrogen data presented are for a single brush and include steady-state performance and preliminary wear data.

Apparatus

Facility Description

Testing was conducted in cell 2 of the Cryogenic Components Laboratory (CCL) at the NASA Lewis Research Center. An aerial photograph of the CCL is shown in figure 1. The test cell, a 4.6- by 4.6-m (15- by 15-ft) expendable building with rollup doors on each side, housed the test article and the associated flow-control and instrumentation hardware. Highpressure liquid hydrogen (LH₂) or liquid nitrogen (LN₂) was fed into the test cell from an adjacent 4.92-m³ (1300-gal), 9.93-MPa (1440-psig) run dewar. This tank was filled from either a 45.42-m³ (12 000-gal) LH₂ low-pressure storage dewar or a 15.14-m³ (4000-gal) LN₂ low-pressure storage dewar, depending on the fluid required, and then was pressurized with gas from two 16.55-MPa (2400-psig), 1982-m³ (70 000-scf) gaseous hydrogen (GH₂) or gaseous nitrogen (GN₂) tube trailers, respectively. These two tube trailers also supplied GN₂ or GH₂ to the test rig turbine drive for the LN₂ and LH2 tests, respectively. After flowing through the test rig, all fluids were vented to the hydrogen burnoff located behind the test cell. All system piping, shown schematically in figure 2, was helium and vacuum purged before each LH₂ test. Gaseous nitrogen was used as the purge gas for LN₂ testing. These tests were controlled remotely from the CCL control room and were monitored using several video cameras, an audio pickup, and the instrumentation systems.

Test Rig Description

The test rig is the Low Thrust Pump Tester designed by Rocketdyne under contract NAS3-23164 (ref. 12) and modified to test brush seals. A cross section of the test rig is presented in figure 3. Note that for clarity some of the ports are shown out of rotation. The Inconel 718 shaft is supported by two pairs of cryogenic ball bearings and is driven by an Astroloy full-admission axial-flow turbine on one end of the shaft. A 50.8-mm-(2.000-in.-) diameter seal runner is located on the opposite end of the shaft. Axial loads are supported by a selfcompensating gas-fed balance piston located at the center of the shaft. Very little axial load is generated by the turbine; most of the axial load is a result of the pressure drop across the brush seal. The balance piston can support axial loads due to a pressure drop across the seal of up to 2.07 MPa (300 psid). Intercavity sealing along the shaft is accomplished using several labyrinth seals.

The tester can accommodate from one to five brush seals in a variety of spacing configurations. The seal holder is 304 stainless steel. Two different Inconel 718 seal runners with a 0.81-µm (32-µin.) surface finish were used: a long, low-speed runner and a short, high-speed runner. The low-speed runner can accommodate all five brushes at one time but is limited to 40 000 rpm to stay below the predicted first critical speed of

45 000 rpm. The high-speed runner, a shortened version of the low-speed runner, accommodates just one seal but can be operated at speeds up to 70 000 rpm, the predicted first critical speed.

Liquid hydrogen or liquid nitrogen was supplied to the inboard, high-pressure side of the runner at pressures up to 5.52 MPa (800 psig), the maximum allowable working pressure of the rig. This supply fluid then passed through a perforated plate, which is integral with the test-seal-end labyrinth seal, to steady the flow. In tests where leakage through the brush seal was low, it was necessary to bypass some flow out of the brush seal supply cavity to keep the rig cold enough. Liquid hydrogen or liquid nitrogen was also supplied to the bearings for coolant. Photographs of the test cell with the rig installed and after it had been chilled are shown in figures 4 and 5, respectively.

Test Hardware

Brush seals are compliant contacting seals. Figure 6 shows a typical brush seal, which comprises a ring-shaped pack of small-diameter wire bristles set at an angle to the radial direction and sandwiched between a front and back washer. The back washer is on the low-pressure side of the seal and serves as a mechanical support to prevent the bristles from bending downstream as a result of the pressure load. Typically, the bristles are designed to have a 127.0- to 254.0-\mu (0.0050- to 0.0100-in.) radial interference with the shaft. Brush seals with an interference leak less than those with a line-to-line or clearance fit (ref. 8). The bristles are angled, usually 30° to 60° and thus act as cantilevered beams. Because of their initial interference with the shaft, the bristles are preloaded and tend to follow the shaft during rotordynamic excursions. The degree to which the bristles follow the shaft, or the frequency response, is important and depends on the radial stiffness of the bristles and mass.

The nominal geometry of the brush seal and runner configurations tested is shown in figure 7. The Inconel 718 seal runner was 50.8 mm (2.000 in.) in diameter and had a surface finish of 0.81 µm (32 µin.) on its outer diameter. The Haynes-25, 0.071-mm- (0.0028-in.-) diameter bristles had a 40° angle to the radius, were packed at a density of 3000 bristles/in.circumference of bore diameter, and had a 127-µm (0.005-in.) nominal radial interference with the runner. The outside diameter of the brushes was 71.60 mm (2.8190 in.) and the axial thickness was 3.61 mm (0.142 in.). Both the front and back washers were made of Hastelloy-X and were 1.42 mm (0.056 in.) thick. The radial clearances between the front and back washers and the runner were 5.08 and 0.279 mm (0.200 and 0.011 in.), respectively. Because there was some slight variation in geometry from brush to brush, the pretest inspection measurements are given in table I. The materials were chosen because they were compatible with liquid nitrogen and hydrogen. The Haynes-25 cobalt-base alloy was used for the bristles because it could

TABLE I.—PRETEST INSPECTION MEASUREMENTS OF BRUSH SEALS AND RUNNERS

Seal identi- fication number		Inside diameter						tside neter			Axial t	hickness	1	
	Front	Front washer Bristles			Back	washer			Front	washer	Back v	washer	Entir	e seal
	mm	in.	mm	in.	mm	in.	mm	in.	mm	in.	mm	in.	mm	in.
1 2 3 4 5	61.06 61.01 61.11 60.99 61.19 61.04	2.404 2.402 2.406 2.401 2.409 2.403	50.60 50.57 50.47 50.47 50.57 50.55	1.992 1.991 1.987 1.987 1.991 1.990	51.44 51.48 51.38 51.44 51.44 51.44	2.025 2.027 2.023 2.025 2.025 2.025	71.63 71.62 71.59 71.60 71.59 71.59	2.8200 2.8197 2.8185 2.8190 2.8187 2.8187	1.35 1.42 1.37 1.45 1.37 1.40	0.053 .056 .054 .057 .054 .055	1.52 1.45 1.37 1.40 1.50 1.40	0.060 .057 .054 .055 .059 .055	3.620 3.627 3.607 3.632 3.627 3.569	0.1425 .1428 .1420 .1430 .1428 .1405

Seal identi- fication number		Radial distance between back washer inside diameter and—				nt inter- e with ner ^a	Bristle					
		inside neter	Runner outside diameter				Hei	ght ^b	Diar	neter	Angle, deg	
	mm	in.	mm	in.	mm	in.	mm	in.	mm	in.		
1 2 3 4 5 6	0.419 .457 .457 .483 .432 .444	0.0165 .0180 .0180 .0190 .0170 .0175	0.320 .345 .295 .320 .320 .315	0.0126 .0136 .0116 .0126 .0126 .0124	0.099 .102 .163 .163 .102 .127	0.0039 .0040 .0064 .0064 .0040 .0050	5.232 5.220 5.321 5.258 5.309 5.245	0.2060 .2055 .2095 .2070 .2090 .2065	0.071	0.0028	37 30 25 38 34 34	

^aLow-speed runner 1 used with seals 1 to 5. High-speed runner 1 used with seal 6. Low-speed runner 1 o.d.: 50.792 to 50.794 mm (1.9997 to 1.9998 in.); high-speed runner 1 o.d.: 50.808 mm (2.0003 in.).

be drawn; the wire diameter was determined by the available die.

Spacers used to study staging effects had the same overall dimensions as the brush seals and an inside diameter that was the same as the front washer inside diameter. Some spacers had radial holes located to match the instrumentation holes in the housing so when that spacer was used, 1.6-mm- (0.06-in.-) diameter thermocouples and pressure tubes could be installed to obtain interstage fluid conditions. Seal positions and instrumentation stations are defined in figure 8(a). Instrumentation was always installed at the entrance and exit of the brush seal cavity, stations 1 and 5, respectively. Figure 8(b) displays the circumferential orientation of the instrumentation.

Configurations Tested

Nine seal configurations were tested and are described in table II. Configurations 1 to 8 were tested in LN_2 and configuration 9 was tested in LH_2 . Configuration (1) was a 12-tooth, 127- μ m- (0.005-in.-) radial-clearance labyrinth seal tested as a baseline with the low-speed rotor in LN_2 . Its axial length is equivalent to five brushes tightly packed, and its geometry is

shown in figure 9. The other configurations were (2) a single brush, (3) two brushes spaced far apart (7.21 mm (0.284 in.), two brush widths between), (4) two brushes tightly packed, and (5) three brushes evenly spaced 3.607 mm (0.142 in., or one brush width between) were tested. Tests of configurations 3 and 5 were repeated and are identified as 6 and 7 in table II: two brushes spaced 7.21 mm (0.284 in.) apart and three brushes evenly spaced. They were repeated because of a problem with the interstage pressure measurements, which is explained in the next section. Then, (8) a single brush was tested to measure static seal performance above 1.21 MPa (175 psid). Finally, in configuration 9, a single brush was tested with the high-speed runner in LH₂.

Instrumentation

The steady-state temperature, pressure, and flow rate of all fluids supplied to the tester were measured along with the seal leakage flow rate and all tester exit temperatures and pressures (see fig. 2). Metal strain gage transducers were used for all pressure measurements. Gold-iron/chromel and chromel/constantan thermocouples were used in the cryogenic liquid

^bRadial length of bristle from front washer inside diameter.

TABLE II.—SEAL CONFIGURATIONS TESTED

Configuration number	Description	Seal position				Seal runner	Test fluid	
		1	2	3	4	5		
1	12-tooth labyrinth			All position	ons	-	Low speed	LN ₂
2	Single brush	Seal 2					1	
3	Two brushes far apart		Seal 3			Seal 4		
4	Two brushes tightly packed			Seal 1	Seal 5			
5	Three brushes evenly spaced	Seal 1		Seal 4		Seal 5		
6	Two brushes far apart; pressure taps at spacer i.d.		Seal 3			Seal 4		
7	Three brushes evenly spaced; pressure taps at spacer i.d.	Seal 1		Seal 4		Seal 5		
8	Single brush; blowout test	Seal 2						
9	Single brush	Seal 6	_				High speed 1	LH ₂

systems and gaseous systems, respectively. All flow rate measurements were made using venturis. Venturis of two different sizes were used in series to measure the brush seal leakage rate.

Four pressure and four temperature measurements each were taken at stations 1 and 5. Two pressure and two temperature measurements could be taken at each of the interstage instrumentation stations 2, 3 and 4. Instrumentation at stations 1 through 5 was located 38 µm (0.0015 in.) from the seal runner in configurations 1 and 2. After testing configuration 2, some thermocouple damage was found and the seal instrumentation was moved back to 76 µm (0.003 in.) from the seal runner. The damage was attributed to insufficient support of the tip in a high flow, causing the tips to bend and break. The interstage pressure tubes were pulled back to the inner diameter of the spacer for configurations 6 and 7 because significant differences between pressure measurements at the same station occurred in configurations 3 and 5 and appeared to be speed dependent. These differences were not seen when the pressure tubes were located at the spacer inside diameter and are thought to be caused by a flow disturbance induced by the pressure tube.

Three eddy-current proximity probes located at 40°, 130°, and 220° were used to monitor seal runner orbits (see fig. 8(b) for orientation). Oscilloscopes displayed the orbits in real time. Two eddy-current proximity probes were used to monitor shaft speed at the single-notched balance piston. Another eddy-current proximity probe was used to monitor the axial shaft motion at the balance piston. An accelerometer was mounted on the seal end of the tester housing to measure radial acceleration to monitor the health of the tester. A complete instrumentation list can be found in appendix A.

Data Acquisition

All steady-state data were recorded using an Escort II data acquisition system that has a sampling rate of 10 kHz. The Escort II system acquires the millivolt data, converts it to engineering units, makes real-time calculations, displays the information on CRT monitors in the control room, and stores the data to the data collector for legal tape storage. The update time is 2 sec. For each steady-state condition, 10 scans of data were recorded. All scans during the static performance test were recorded. Once recorded, the data were sent to the scientific VAX cluster for postprocessing.

Dynamic data from the eddy-current proximity probes and accelerometer were recorded on a 14-channel FM tape recorder. The time code was recorded on channel 14 to enable correlation of the dynamic data with the steady-state data. A bandwidth of 62.5 kHz was used with a tape speed of 381 mm/ sec (15 in./sec). Capacitors (1 μF) filtered out the dc offset of the proximity probe signals to bring them into the 1.0-V peak range of the tape recorder. Four oscilloscopes were used to monitor seal runner orbits, vibration, and speed signals.

In addition to the Escort CRT monitors and oscilloscopes, digital panel meters were used to display certain control and abort parameters, as shown in figure 10. A stop-shaft-rotation abort would be triggered by any of the following conditions: excessive shaft speed, excessive axial shaft motion, or excessive pressure at the turbine inlet.

Test Procedure and Nominal Operating Conditions

After the appropriate facility purges and setup, the seal tester was chilled down by flowing the cryogenic test fluid to the bearings and seal cavities. When liquid temperatures in the tester had been reached, approximately 77.8 K (140 R) for LN₂ and 27.8 K (50 R) for LH₂, testing began. Nominal inlet pressures were 5.38 to 5.5 MPa (780 to 800 psig) for LN_2 and 2.8 to 3.4 MPa (400 to 500 psig) for LH₂ tests. The outlet pressure of the seal was kept well above the critical pressure to avoid two-phase flow. The pressure drop across the seal package was set by controlling the backpressure on the seal cavity. Temperatures throughout the tester were monitored closely. A significant temperature rise indicated that the test fluid had run out.

Labyrinth Seal LN₂ Tests

1.38

1.65

2.07

System checkout tests were conducted with the labyrinth seal installed in the tester. A maximum shaft speed of 38 000 rpm

200

225

300

was obtained at zero pressure drop across the seal. At 0 rpm, a maximum pressure drop across the seal of 2.24 MPa (325 psid) was obtained. Baseline leakage performance of the labyrinth seal was measured for pressure drops across the seal of 0.17 to 2.07 MPa (25 to 300 psid) at shaft speeds of 0, 5, 15, 25, and 35 krpm. A few intermediate test conditions at 10, 20, 30, and 31 krpm were also recorded, as indicated in table III(a).

Brush Seal LN₂ Tests

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Prior to any shaft rotation, the LN₂ brush seal leakage rate was measured for increasing and then decreasing pressure drops across the seal of 0, 0.17, 0.52, 0.86, 1.03, 1.21, 1.03, 0.86, 0.52, 0.17, and 0 MPa (0, 25, 75, 125, 150, 175, 150, 125, 75, 25, and 0 psid). Then the pressure drop across the seal was set to 0.17 MPa (25 psid) and the shaft speed was increased to 5000 rpm. Again, data were taken for increasing and decreasing pressure drops across the seal in the same order and at the same levels as at 0 rpm, with the exception of the 0-MPa (psid) point. Because of balance piston limitations, the 0-MPa (psid)

TABLE III.—TEST MATRIX FOR LABYRINTH AND BRUSH SEALS IN LIQUID NITROGEN AND IN LIQUID HYDROGEN

(a) Labyrinth seal in liquid nitrogen

Seal pre	essure drop					Shaft spee	ed, a rpm			
MPa	psid	0	5000	10 000	15 000	20 000	25 000	30 000	31 000	3.
0	0			1		V		1		
0.17	25	√.	√		7		√		√	
0.52	75	√	V		V		. √		√	
		1	T			T	1	i 1		

MPa	psid	0	5000	10 000	15 000	20 000	25 000	30 000	31 000	35 000
0	0			1		1		1		√ √
0.17	25	1	√		7		√		V	√
0.52	75	1	V		V		√		V	√
0.86	125	1			√		1	√		√
1.02	150	1	al.		J		V	J		V

√

V

V

 $\sqrt{}$

V

V

Seal pres	ssure drop		Shaft speed, rpm											
MPa	psid	0	5000	0	15 000	0	25 000	0	35 000	0				
0	0	1		1		1		1		4				
0.17	25	1	1	1	√	1	1	1	1	1				
0.52	75	1	√ √	1	1	1	4	1	√ √	1				
0.86	125	1	√	1	V	√	√	1	√	7				
1.03	150	4	√	1	7	√	√	1	1	1				
1.21	175	1	√	4	√	V	√	1	V	. √				
1.03	150	4	√	1	√	7	V	√	√	4				
0.86	125	√	√	√ _	√	1	V	1	√	√				
0.52	75	1	1	1	√	1	1	√	1	√				
0.17	25	1	1	√	1	1	V	√	1	√				
0	0	√		V		1		1		1				

³²⁵ Shaft speeds of 34 000, 37 000, and 40 000 rpm were also tested.

condition could not be reached during shaft rotation. The shaft was then brought down to 0 rpm and data were taken as the pressure drop was varied from 0 to 1.21 to 0 MPa (0 to 175 to 0 psid). Data were taken in a similar manner for 15 000-, 0-, 25 000-, 0-, 35 000-, and 0-rpm shaft speeds. The repeated data at 0 rpm were taken to determine if wear of the brush or runner had occurred. The specific test conditions for the single brush seal (configuration 2) are given in table III(b). For multiple brush configurations, the procedure was the same, except that the maximum total pressure drop was greater—up to 1.9 MPa (275 psid). However, the pressure drop across any individual brush seal did not exceed 1.21 MPa (175 psid). Each test condition was held for approximately 80 sec.

An additional static seal performance test was conducted for a single brush in LN₂. The purpose of the test was to determine the leakage performance for high-pressure (>1.21 MPa or 175 psid) drops across the seal and to verify that a seal blowout would not occur. The expected indication of a seal blowout, a condition in which the bristles bend downstream and lift off the shaft, is a sudden increase in leakage rate. After the tester was chilled down, a 0.59-MPa (85-psid) pressure drop across the seal was applied and the shaft speed was increased to 5000 rpm. At this low speed, the pressure drop across the seal was increased to 1.2 MPa (170 psid) and then decreased to 0.59 MPa (85 psid). Next, the shaft speed was brought to zero, and then the pressure drop across the seal was brought to zero. This sequence was used to properly seat the seal before starting the static performance test. At 0 rpm, while data were continually recorded, the pressure drop across the seal was increased to a maximum of 4.6 MPa (670 psid). Then the pressure load was gradually removed. Unfortunately, the leakage rate instrumentation reached a maximum limit at 3.8 MPa (550 psid) across the seal.

Brush Seal LH₂ Tests

Only configuration 9, a single brush on the high-speed runner, was tested in LH_2 . The procedure for the LH_2 tests was somewhat different from that for the LN_2 tests; primarily, the differences were that the high-shaft-speed data were taken first and the maximum shaft speed was 65 000 rpm.

First, to check out the system and obtain baseline leakage data for the seal, the pressure drop across the seal was varied from 0 to 1.21 MPa (0 to 175 psid) and then decreased to 0 MPa (0 psid) at a shaft speed of 0 rpm. Second, tests were conducted to determine the maximum shaft speed for the high-speed seal runner. At a pressure drop across the seal of 0.52 MPa (75 psid), the speed was increased and data were recorded at 15, 25, 35, 45, 55, 65, and 75 krpm. A maximum shaft speed of 65 000 rpm was chosen to conduct the seal leakage performance tests. At 65 000 rpm the pressure drop across the seal was varied and data were taken in the order of the following conditions: 0.52, 0.69, 0.83, 1.08, 1.21, 1.08, 0.83, 0.69, 0.52, and 0.17 MPa (75, 100, 121, 156, 175, 156, 121, 100, 75, and 25 psid). This speed

and these pressure conditions were selected to match the design conditions of the brush seal to be used in the Advanced Expander Test Bed LH₂ turbopump (ref. 13). The shaft speed was then decreased to 0 rpm and data were taken as the pressure across the seal varied from 0.17 to 1.21 MPa (25 to 175 psid) and then decreased to 0 MPa (0 psid). Data were then taken at shaft speeds of 55 000, 0, 45 000, 35 000, 25 000, 15 000, and 0 rpm at the pressure conditions given in table III(c). Again, each test condition was held for approximately 80 sec.

Calculations

With the exception of the static performance test data, all data presented are an average of 10 scans. Prior to averaging, each scan was reviewed to ensure that steady-state conditions existed and that averaging was appropriate. The temperatures and pressures at each seal instrumentation station were also averaged. Pressure and temperature differences between stations were calculated from average values. Standard venturi equations were used to calculate flow rates (ref. 14). Actual fluid properties were obtained from the program FLUID (ref. 15). To account for variations in inlet conditions, a parameter called RODPab was calculated. RODPab is the inlet density at station a multiplied by the pressure difference between station a and station b. The power loss across the seal was calculated as the seal leakage mass flow rate multiplied by the enthalpy difference of the fluid across the seal. The measurement uncertainties of key seal performance parameters were calculated and are presented in appendix B.

Prediction Tools

Computer analysis codes were used to predict the performance of the labyrinth and brush seals. The code used to predict the labyrinth seal performance was developed at Texas A & M University under NASA Contract NAS8-34536. The code calculates mass leakage rate for incompressible fluids in straight-through labyrinth seals using Dodge's formula and interpolating experimental data (ref. 16). In making the leakage predictions with this code, the measured fluid conditions were used for each data point. The fluid properties data required for input were obtained using a program called GASPROPM, a user-friendly front end for the fluid properties routine called FLUID (ref. 15).

Analysis techniques to predict brush seal leakage performance are less developed than those used for labyrinth seal analysis. The brush seal is more difficult to model because of its compliant and permeable nature. Theories developed for crossflow in tube bundles and for flow-through porous mediums have been applied to brush seals to account for the flow resistance of packed, compliant bristles.

Chupp, Holle, and Dowler (ref. 17) developed a simple flow model that uses a single parameter, effective brush thickness, to correlate flow through the seal. The underlying model is based

(c)	Rmich	seal	in	lionid	hydrogen

Seal pres	sure drop			(-) -			eed, b rpm		• • • • • • • • • • • • • • • • • • • •		
MPa	psid	0	65 000	0	55 000	0	45 000	35 000	25 000	15 000	0
0.07	10	1									
0.10	15					V				√ √	1
0.17	25	1		1	√	7	√	√	1	√	√
0.34	50	1									
0.52	75	√	√	1	√	1	1	1	√	√	√
0.69	100	√	√								
0.83	121		√								
0.86	125	√		√	√	1	1	√	√	√	√
1.03	150	1			√	√	√	√	√	√	√
1.08	156		√								
1.21	175	1	√	1	√ _	1	1	1	1	√	1
1.08	156		V								
1.03	150	√			√	√	√	√	√	√	√
0.86	125	1		√	√	√	√	1	√	√	√
0.83	121		√								
0.69	100	4	√								
0.52	75	√	√	√	√	1	. √	1	√	√	- √
0.34	50	1									
0.17	25	1	1	1	√	√	√	√	√	√ √	√
0.10	15				√	1		√	√		1
0.07	10	1									
0	0	1				1					√

^bAt each shaft speed, data were taken at seal pressure drops as listed from top to bottom; shaft speeds were run in sequence as listed from left to right.

on crossflow through staggered tubes. The simple model reveals the active nature of a brush seal as the pressure drop changes. A more comprehensive flow model was proposed by Hendricks et al. (ref. 18). Hendricks' bulk flow model is also based on theory that deals with crossflows in bare and extended tubes. This brush seal flow model predicts leakage rates by using brush seal geometry, seal pressure drop, and fluid transport properties as inputs. Hendricks reported that the model predicted trends and general levels reasonably, but at low flows and low pressure drops, the model deviated from experimental data provided by Cross Manufacturing.

Another approach, proposed by Chew from Rolls Royce, suggested the use of the Ergun equation:

$$\Delta P = aq + bq^2 \tag{1}$$

where ΔP is the pressure drop across the seal; a and b are coefficients; and q is the volumetric flow rate. The equation was originally formulated to predict fluid flow through porous materials. The permeability of the brush seal bristles can be considered a porous medium. However, the bristle compliancy complicates the flow problem and is not captured by the Ergun

equation. On the other hand, in a letter to Hendricks (J.W. Chew, Rolls-Royce Aerospace Group, P.O. Box 31, Derby DE288J, England, October, 27, 1992), Chew's prediction showed good correlation with data provided by Hendricks (ref. 19). Hendricks has further investigated the use of the Ergun equation and has developed relations for the coefficients used in the equation (ref. 20). He proposed that the coefficients be a function of brush porosity, brush thickness, bristle diameter, fluid viscosity, density, and turbulence friction factor. Predictions from Hendricks, Flower, and Howe (ref. 20) showed good correlation with gaseous helium, air, argon, and carbon dioxide brush seal data obtained by Carlile, Hendricks, and Yoder (ref. 19). When Hendricks applied the Ergun equation to data for brush seals tested in liquid nitrogen (ref. 10), the correlation was not as good.

Kudriavtsev and Braun (ref. 21) proposed solving the continuity and momentum equations for flow patterns around sets of pins to simulate flow patterns in brush seals. To reduce computer memory and power requirements necessary to model a full brush seal, Kudriavtsev suggested using representative segments. A few columns and rows of bristles may adequately represent a whole seal if proper boundary conditions are specified. In addition, Kudriavtsev assumed that the first and

last couple rows of bristles for a brush seal of 10 or more rows could be neglected because they tend to spread and do not significantly effect the fluid pressure drop. Kudriavtsev explored this approach and reported that it was feasible. Much work, however, is still needed to fully develop it.

The proposed models have been developed mainly for gas brush seals because gas turbine engines are the prime applications. Consequently, ample gas brush seal data are available. However, little data exist for brush seals operating in liquid environments. Although gradually changing, there are insufficient data to calibrate and validate the brush seal models for liquid applications. Because more experimental data are required, no analytical comparisons are presented.

Results and Discussion of LN₂ Tests

Temperature, pressure, speed, and leakage rate data for all configurations are presented in appendixes C and D in SI and English units, respectively.

Labyrinth Seal Performance

A 12-tooth, 127- μ m- (0.005-in-.) radial-clearance labyrinth seal was tested in liquid nitrogen to establish a baseline for comparison. The measured and predicted mass leakage rates of the labyrinth seal are shown in figure 11 as a function of the inlet density ρ multiplied by the pressure drop ΔP across the seal for all shaft speeds tested. The pressure drop across the seal was multiplied by the inlet density to account for the variation in the inlet conditions from test to test. The data show no appreciable speed effect on the leakage rate, and the measured and predicted leakage rates are of the same magnitude and trend, increasing with increased $\rho\Delta P$.

Single Brush Seal Performance

The leakage performance of a single brush seal in liquid nitrogen located in position 1 of the seal cartridge is shown in figure 12. Again, mass leakage rate is plotted as a function of the inlet density multiplied by the pressure drop across the seal for all shaft speeds. It is interesting to note that the first leakage rate data taken at 0 rpm is approximately 1.7 times greater than all the other data. This phenomenon was seen in each new configuration and indicates that both a pressure load and shaft rotation are required to seat the seal bristles into their optimum position. Although the leakage data for the different shaft speeds exhibit some variation, there is no distinct speed dependence. However, the leakage rate at the end of the test was approximately double that measured at the beginning, which indicates that wear had occurred. Figure 13 compares the leakage performance of the labyrinth and the brush seals and shows that the single brush seal had a mass leakage rate of onehalf to one-third that of the 12-tooth labyrinth seal with a radial clearance of 127 μm (0.005 in.).

Figure 14 shows fluid temperature rise across a single brush seal in liquid nitrogen between stations 1 and 3 as a function of $\rho\Delta P$ for the shaft speeds tested. As expected, the fluid temperature rise is greater at higher shaft speeds, mainly because of higher frictional heating. The fluid viscous shear forces also generate more heat at higher shaft speeds. The temperature rise decreases for increased $\rho\Delta P$ because there is more coolant flow to carry the heat away.

The results of the static seal performance test are shown in figure 15 in which leakage rate is plotted as a function of $\rho\Delta P$. A pressure drop across the seal of 3.8 MPa (550 psid) was obtained with no evidence of blowout occurring.

The power loss for a single seal in position 1 was calculated as the product of the seal mass leakage rate and the fluid enthalpy change from station 1 to station 2. In figure 16 the power loss is plotted as a function of the shaft speed for several ΔP values. Although higher ΔP conditions appear to increase power loss slightly, the variation is within the uncertainty of this calculation. The uncertainty is strongly influenced by the sensitivity of enthalpy to temperature changes. Power loss is, however, a function of speed cubed. The maximum power loss measured for a single brush was $1826 \,\mathrm{W}\,(2.45 \,\mathrm{hp})$ at 35 000 rpm and a pressure drop across the seal of 1.21 MPa (175 psid). Labyrinth seal power loss measurements are not provided for comparison because the thermocouples at station 5 were located in a relatively large cavity and were exposed to environmental heat loads not attributable to the seal.

Staging Effects

Staging effects on leakage rate are significant, as seen in figure 17. In this figure, the leakage rate at a shaft speed of 5000 rpm is plotted against $\rho\Delta P$ for a single brush, for two brushes far apart (7.21 mm or 0.284 in.), and for two brushes tightly packed. The leakage rate for two brushes far apart is approximately one-half that of the single brush leakage rate. However, the leakage rate for two brushes tightly packed is approximately three-fourths that for the single brush seal. This phenomenon of two brushes far apart leaking less than two brushes tightly packed occurred at all shaft speeds (5, 15, 25, and 35 krpm). Additional brushes caused the fluid temperature rise across the seal to increase because the added brushes caused more frictional heating. Figure 18 compares the fluid temperature rise between stations 1 and 5 for one, two, and three brushes as a function of $\rho\Delta P$ at 35 000 rpm. The maximum temperature rise of approximately 53 K (95 R) occurred for three brushes at the lowest $\rho\Delta P$ value, which is also the lowest flow rate. It is important to note that the fluid temperature measured at station 5 is really that of the seal leakage mixed with the fluid in the exhaust cavity, which tends to be somewhat warmer. Therefore, the actual temperature rise is something less than the values shown in figure 18.

The pressure load distribution in a multistage configuration appears to be affected by shaft speed. Plots of leakage performance versus $\rho\Delta P$ for individual brushes and for all brushes together in the configuration three brushes evenly spaced are shown in figures 19 and 20 at 0 and 35 000 rpm, respectively. At 0 rpm, the first and second brushes each carried approximately 25 percent of the total pressure drop across the seal, and the third brush seal carried the remaining 50 percent. At 35 000 rpm, each of the three brushes carried approximately equal portions of the total pressure drop. A review of the data at 5, 15, and 25 krpm shows a gradual transition of the pressure load distribution between 0- and 35 000-rpm shaft speeds.

Preliminary Wear Data

Brush seal wear is affected by many parameters: material properties and combination, surface finish, geometry, shaft speed, friction coefficient, shaft rotordynamics, initial interference, and coolant flow. The Inconel 718 rotor had a surface finish of $0.81 \, \mu m$ (32 μin .). Shaft rotordynamics were very good with a nominal seal runner orbit of less than 5 μm (0.0002 in.) in diameter. A maximum seal runner orbit diameter of 25 μm (0.001 in.) occurred at 35 000 rpm for a short period of time when the pressure drop across the seal was being adjusted. No significant vibration was observed. The maximum shaft speed was 35 000 rpm, which translates to a surface velocity of 93 m/sec (305 ft/sec). Again, the bristle material was Haynes-25.

Seal runner wear did occur as evidenced by the tracks found during posttest inspection. A scanning electron microscope (SEM) photograph of the tracks is shown in figure 21. To measure runner wear, profilometer traces were taken across the axial length of the runner at four circumferential locations: 0°, 90°, 180°, and 270°. The profilometer trace at 0°, taken after testing configuration 4 before any track was reused, is shown in figure 22. The final profilometer trace, taken after testing configuration 7, is shown in figure 23. The maximum groove depth measured was 25 µm (0.0010 in.) and the nominal groove depth measured was 19 µm (0.00075 in.) after 4.31 hr accumulated shaft rotation time. A plot of the maximum groove depth of each track as a function of time is shown in figure 24. The maximum, minimum, and average values of the maximum groove depth measurements are shown. Tracks 1 and 3 show first an increase and then a decrease in groove depth with time. Track 5 shows a decrease in groove depth with time but reveals variations in the depth measurement of 11 μ m (4.5×10⁻⁴ in.). The other tracks have a variation in the groove depth measurement of approximately $3 \mu m (1.2 \times 10^{-4} in.)$. The wear tracks had an axial width up to 1.2 mm (0.049 in.). This is larger than the bristle pack width of 0.76 mm (0.0298 in.). The difference between the bristle pack width and the track width is greater than the measured axial motion of the shaft of 0.51 mm (0.020 in.). Because there was some axial motion so that the brushes did not run over the exact spot on the runner all the time and because the shaft speed varied, it is valuable to look at wear rate in terms of groove area and distance, as shown in figure 25. This view of the wear data shows more consistently an increase in wear with an increase in distance. The maximum distance was 805 km (2.64 million ft).

The bristles also show wear of approximately 25 to 76 µm (0.001 to 0.003 in.). Bristle wear is difficult to quantify because of uncertainty in the bristle bore diameter measurement. An optical comparator was used to measure the inner diameter of the brush seals and, depending on the exact circumferential location and the person taking the reading, variations of 191 μm (0.0075 in.) were found. These measurements were also affected by unevenness of the bristles, as shown in figure 26. Early in the test matrix, approximately 10 bristles showed evidence of some melting (see fig. 27). Melted bristles were first found after running high-speed conditions with no ΔP across the seal. This implies that some leakage is necessary to cool the bristles and that high-temperature bristle materials may need to be used. Once bristle melting was discovered, these high-speed and no-flow test conditions were discontinued. It also appears that the wear is substantially more on the downstream bristles than on the upstream bristles, as shown in figure 28. The bristles in region A are the downstream bristles that are close to the back washer and show a smearing-type wear. Bristles in region B show little, if any, wear.

Results and Discussion of LH₂ Tests

Performance Data

The leakage performance of a single brush in liquid hydrogen at all speeds tested is shown in figure 29 and is compared with the predicted leakage performance of a 12-tooth, 127-µm-(0.005-in.-) radial-clearance labyrinth seal at 0 and 65 000 rpm. Unlike the liquid nitrogen data, the brush seal leakage performance is not significantly better than the predicted labyrinth seal leakage performance, and a speed effect is present. As speed decreased from 65 000 to 35 000 rpm, the leakage rate decreased slightly. Then a jump occurred at 25 000 rpm, with the leakage rate increasing to values approximately 50 percent larger than the leakage rate at 65 000 rpm. As the speed decreased further to 15 000 rpm, the leakage rate again decreased but still remained higher than the data taken at 65 000 rpm. Although no definitive explanation for these observations can be given at this time, possible causes include wearing of the bristles and lifting away of the bristles from the shaft as a result of shaft orbits or aerodynamic effects. Other studies have found that bristle hysteresis and stiffening effects can significantly affect seal performance (ref. 22), and it is likely that these are contributing factors. The final data taken at 0 rpm has leakage rates one-half to one-third of the predicted labyrinth seal leakage rates. More data need to be taken to confirm this result. It is possible that the bristles relaxed and packed themselves more tightly when the pressure drop across the seal was decreased to 0.07 MPa (10 psid).

As shown in figure 30, the fluid temperature rise between stations 1 and 2 at all speeds and $\rho\Delta P$ values was minimal, with a maximum temperature rise of approximately 11 K (20 R). Although this is substantially less than the temperature rise in liquid nitrogen, it is not surprising. Comparing the nominal inlet conditions of LH₂ and LN₂ reveals that the specific heat of hydrogen is approximately five times greater than that of liquid nitrogen.

The power loss of a single brush seal in liquid hydrogen is shown in figure 31 as a function of shaft speed for two pressure drops across the seal, 1.21 and 0.52 MPa (175 and 75 psid). As observed in the liquid nitrogen data, the higher pressure drop across the seal has a slightly higher power loss and the power loss is a function of speed cubed. The maximum power loss in liquid hydrogen was 2180 W (2.92 hp) and occurred at 65 000 rpm at a pressure drop across the seal of 1.21 MPa (175 psid). As expected, the power loss in liquid nitrogen was greater than in liquid hydrogen largely because of the greater viscosity and lower specific heat of liquid nitrogen. Specifically, the power loss in LN₂ is 1827 W (2.45 hp) and in LH₂ is approximately 634 W (0.85 hp) at 35 000 rpm at a ΔP of 1.21 MPa (175 psid).

Preliminary Wear Data

The bristle and seal runner materials were the same as those used in the liquid nitrogen tests: Haynes-25 bristles and Inconel 718 runner. The shaft rotordynamic excursions were small, with a maximum orbit diameter of 57 μm (0.00225 in.) occurring at 65 000 rpm (a surface velocity of 172.9 m/sec or 567.2 ft/sec). It should be noted that during system checkout testing there were two occurrences of momentary overspeeds in excess of 80 000 rpm. A total of 1.8 hr of shaft rotation time was accumulated. This is a linear distance of 869 km (2.85 million ft). Although the accumulated shaft rotation time in liquid hydrogen was less than in the liquid nitrogen tests, the accumulated linear distance was approximately 8 percent more.

Posttest examination revealed no wear of the runner but instead, a deposit of bristle material on the runner (shown in fig. 32). The bristle interference, 127 µm (0.005 in.) radially, had been totally consumed. This result is significantly different from the wear found in LN₂. However, there were two major differences in the tests. First, hydrogen is a reducing environment and nitrogen is inert. Second, the hydrogen testing was done at shaft speeds nearly double those of the nitrogen testing. Although intuition suggests that the shaft speed is more likely the key factor, further testing is required. An SEM photograph of the bristle tips (fig. 33) shows a smearing type of wear. Also, the outer bristles on each side of the brush pack were bent out axially whereas the bristles towards the center of the brush appeared to be uniformly packed, as shown in figure 34. The

outer bristles also exhibited circumferential bending as well (see fig. 35).

Concluding Remarks

The compliant contacting nature of brush seals gives them a very small effective clearance. Both a pressure load and shaft rotation were required to initially seat the seal bristles in their optimum position. The measured liquid nitrogen (LN₂) leakage of a single brush seal was one-half to one-third the leakage of a 12-tooth labyrinth seal. Predictions of the labyrinth seal LN₂ leakage were in agreement with the measured data. The leakage performance of a single brush seal in liquid hydrogen (LH₂) was comparable to that in liquid nitrogen. However, the LH₂ leakage was expected to be less because of the lower density of LH₂. In comparison with predicted LH₂ leakage performance for a 12-tooth, 127-um- (0.005-in.-) radial-clearance labyrinth seal, the single brush leakage was the same. Also, in LN₂, leakage did not depend on shaft speed but in LH₂, a speed dependence was observed. It is possible that significant wear occurred early in the LH2 tests and that the bristles lifted off the rotor. Another possible explanation for this observed speed dependence is that LH2 testing was conducted at higher shaft speeds where shaft orbits were larger and that a clearance opened between the bristles and the runner. This may be combined with a hysteresis effect. Hysteresis effects have been observed in hot gas brush seal studies. During LH2 testing, the pressure load on the seal was not reduced to nearly zero between each shaft speed tested, as done in the LN₂ testing.

As expected, the fluid temperature rise across the seal is a function of the leakagé rate and the shaft speed. A pressure drop across the seal of 3.8 MPa (550 psid) was applied at 0 rpm with no blowout of the seal. The pressure capability of brush seals is certainly a function of the seal geometry and may be quite high. However, further testing is needed at both static and rotating conditions. The power loss in LN₂ was greater than in LH₂ because of the greater viscosity of LN₂. However, in either fluid the power loss was small: 1827 W (2.45 hp) in LN₂ and 634 W (0.85 hp) in LH₂ at 35 000 rpm at a pressure drop across the seal of 1.21 MPa (175 psid). The maximum power loss in LH₂ was 2180 W (2.92 hp) at 65 000 rpm at a pressure drop across the seal of 1.21 MPa (175 psid).

Staging effects are significant. In LN_2 , two brushes far apart (spaced 7.21 mm or 0.284 in.) leaked less than two brushes tightly packed. In the three-brushes-evenly-spaced configuration, the pressure load was not always split evenly between the seals. The split of the pressure load seemed to depend on the shaft speed. Further testing is needed to fully understand staging effects.

After accumulating 4.31 hr of rotordynamically stable shaft rotation time in liquid nitrogen, the Inconel 718 shaft had a maximum groove depth of 25 µm (0.001 in.), and the Haynes-25

bristles had worn 25 to 76 μ m (0.001 to 0.003 in.). However, in LH₂ the bristle wear was substantially worse, consuming the entire initial radial interference of 127 μ m (0.005 in.) after accumulating 1.8 hr of shaft rotation time. It is important to recognize that the time at which the bristle wear occurred during this 1.8 hr is unknown. The greater wear in LH₂ may be attributed to the higher shaft speeds, an effect of the hydrogen environment, or both. Because bristle material transferred onto the runner and there was no wear of the runner in liquid hydrogen, it is possible that the higher shaft speeds used in the LH₂ testing raised the bristle temperature enough to substantially reduce its shear strength, allowing the bristle material to smear. It is also possible that hydrogen, a reducing agent, acts

as a catalyst to weld the similar materials within the brush and rotor materials. Further testing is needed to fully understand the wear mechanisms and to investigate several runner coatings that may alleviate the wear problem in LH_2 . Additional leakage performance data are also needed to calibrate and validate analytical models of brush seals for cryogenic applications.

Lewis Research Center National Aeronautics and Space Administration Cleveland, Ohio, April 10, 1996

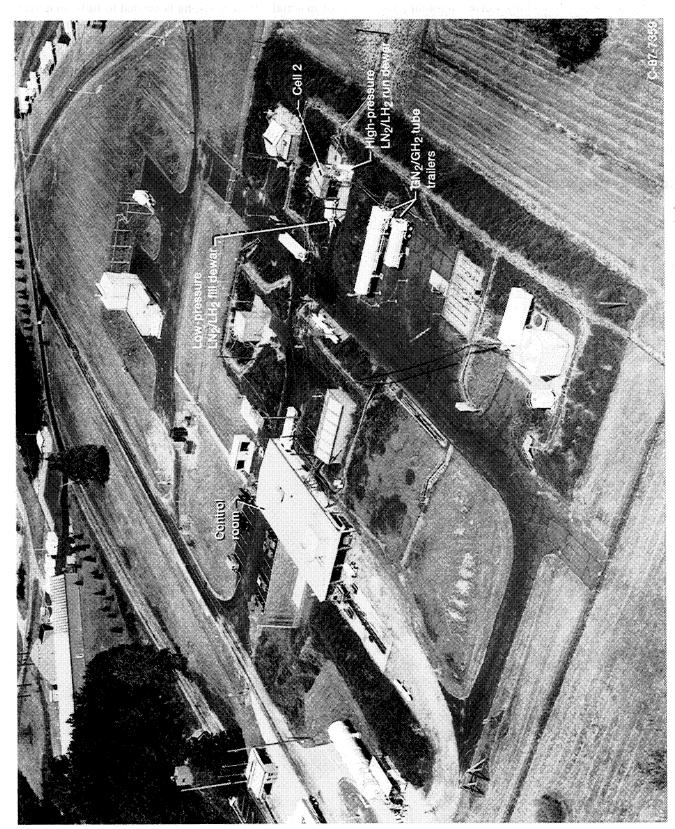
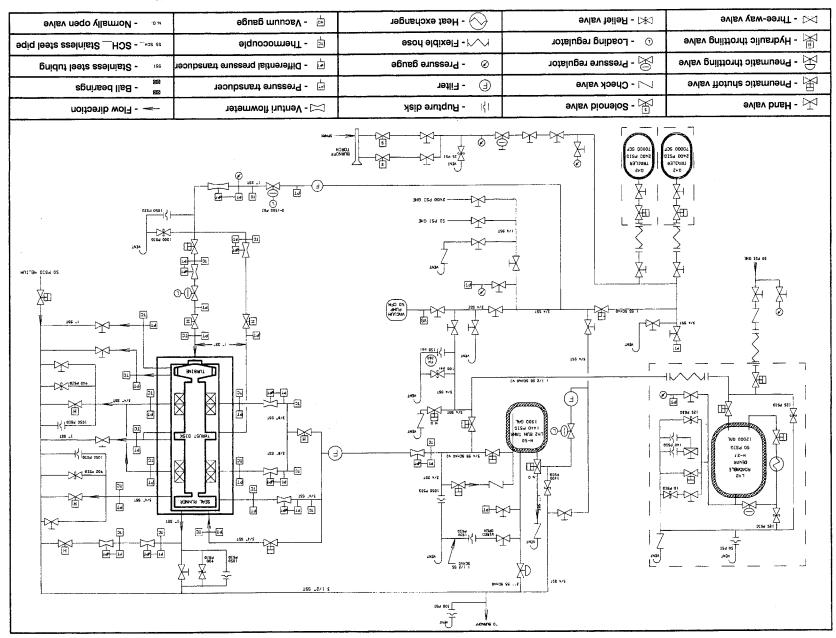


Figure 1.—Cryogenics Components Laboratory (CCL) at the NASA Lewis Research Center.

Figure 2.—Brush seal liquid hydrogen (LH₂) test piping. (All pressures are in psig unless noted.)



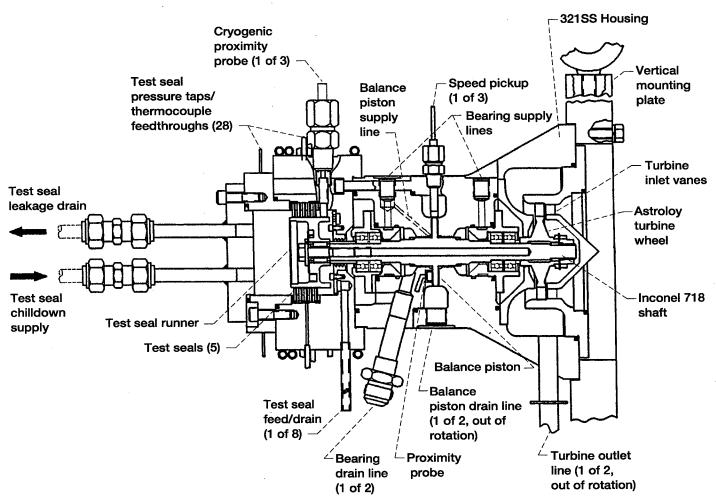


Figure 3.—Cross section of Cryogenic Brush Seal Tester. (Some parts shown out of rotation for clarity.)

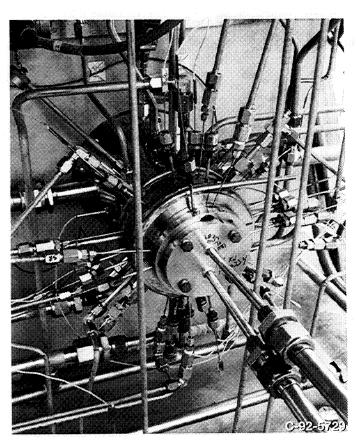


Figure 4.—Cryogenic Brush Seal Tester installation.

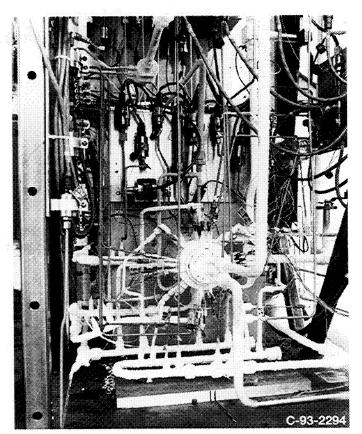


Figure 5.—Cryogenic Brush Seal Tester during test.

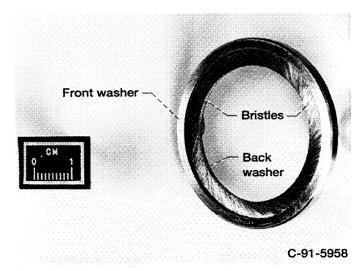


Figure 6.—Typical brush seal.

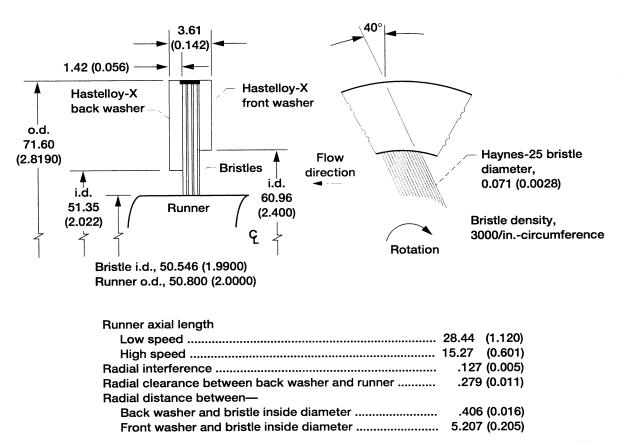
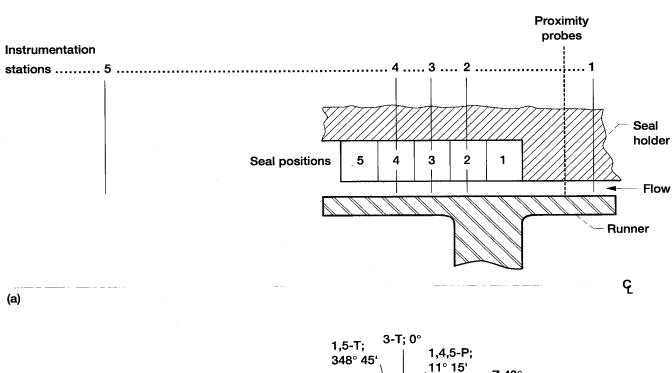


Figure 7.—Nominal brush seal and runner geometry. (Not to scale; all dimensions are in mm (in.).)



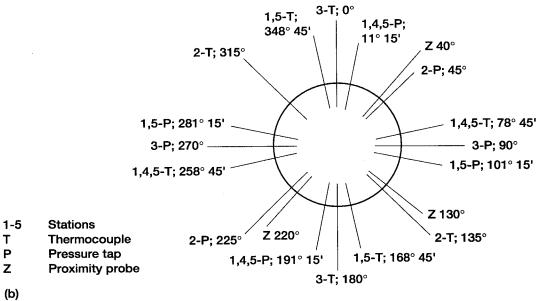


Figure 8.—Location of brush seal positions and instrumentation stations. Low-speed runner shown. (a) Axial locations. (b) Circumferential locations. View looking from seal end.

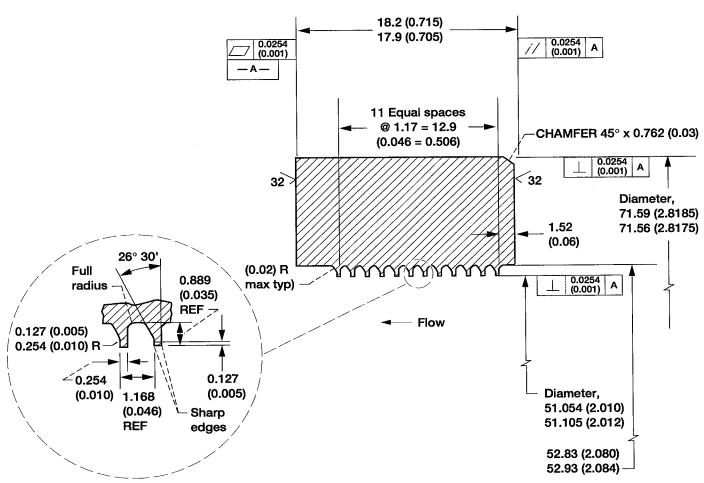


Figure 9.—Labyrinth seal geometry; material, Inconel 718. Dimensions in mm (in.).

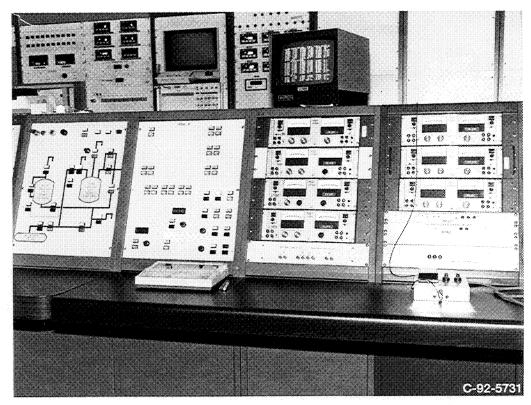


Figure 10.—Control panel for cryogenic brush seal testing.

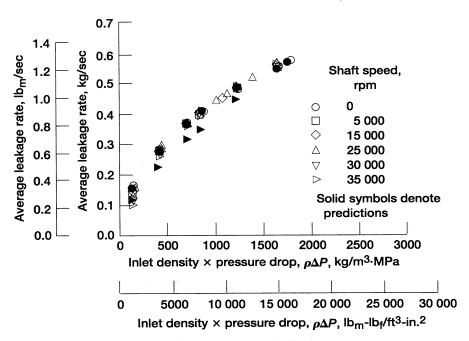


Figure 11.—Comparison of predicted and measured average LN_2 leakage rate through 12-tooth labyrinth seal as function of inlet density times pressure drop across seal for configuration 1 at several shaft speeds. Seal radial clearance, 127- μ m (0.005-in.); seal runner outside diameter, 50.794 mm (1.9998 in.).

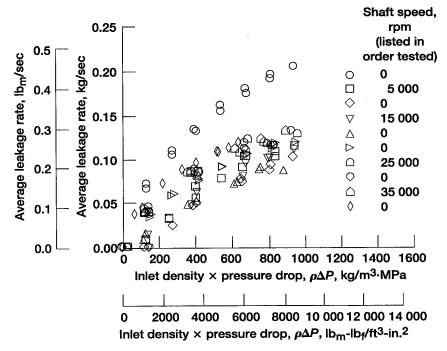


Figure 12.—Average LN₂ leakage rate for single brush seal with initial radial interference of 0.102 mm (0.004 in.) as function of inlet density times pressure drop across seal for configuration 2 at all speeds tested.

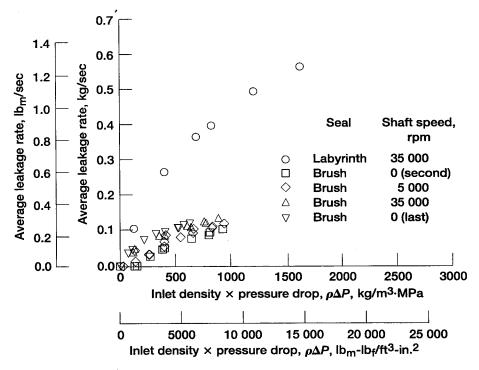


Figure 13.—Comparison of 12-tooth labyrinth seal and single brush seal LN₂ leakage performance. Labyrinth seal radial clearance, 0.127- μ m (0.005-in.); brush seal initial radial interference, 0.102 mm (0.004 in.).

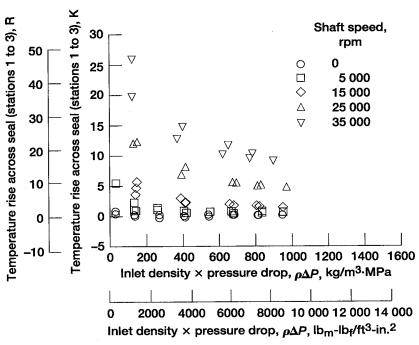


Figure 14.—Effect of speed on LN₂ temperature rise across single brush seal (stations 1 to 3) as function of inlet density times pressure drop across seal for configuration 2.

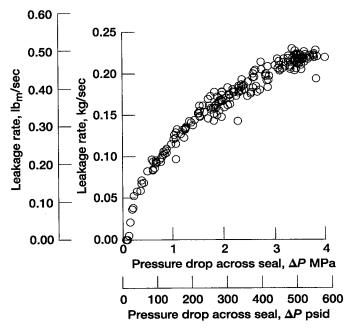


Figure 15.—LN₂ leakage rate as function of pressure drop across single brush seal during static performance test for configuration 8 at 0 rpm.

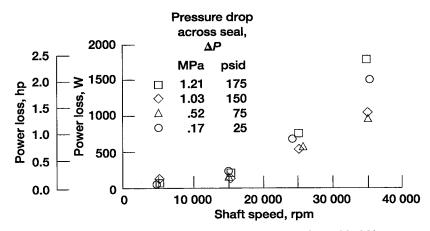


Figure 16.—Power loss to fluid across single brush seal in LN_2 as function of shaft speed for configuration 2.

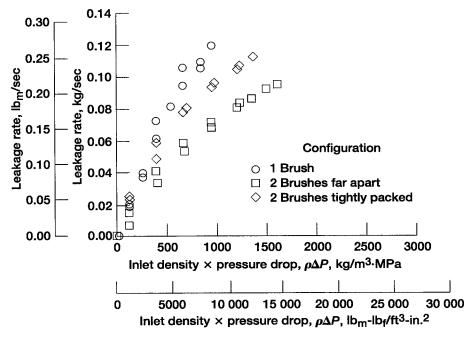


Figure 17.—Comparison of ${\rm LN}_2$ leakage rate of one- and two-brush seals in configurations 2 to 4 at 5000 rpm.

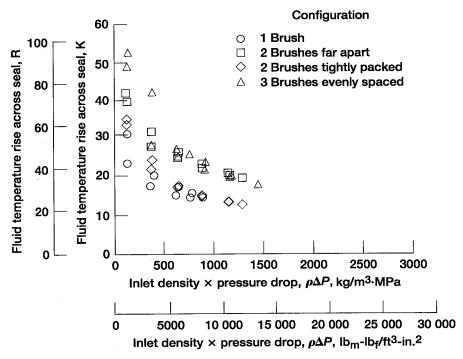


Figure 18.—Effects of staging on fluid temperature rise across seal in LN_2 for configurations 2 to 5 at 35 000 rpm.

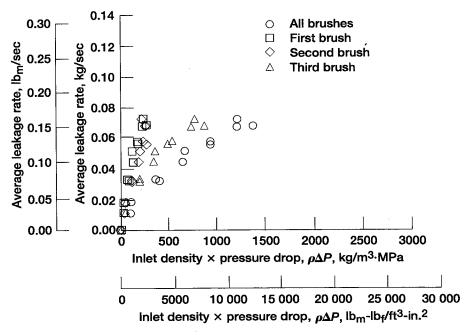


Figure 19.—LN₂ leakage performance of each stage and of all stages for three brushes evenly spaced (configuration 7) at 0 rpm.

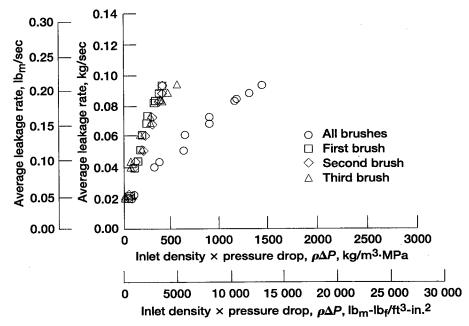


Figure 20.—LN₂ leakage performance of each stage and of all stages for three brushes evenly spaced (configuration 7) at 35 000 rpm.

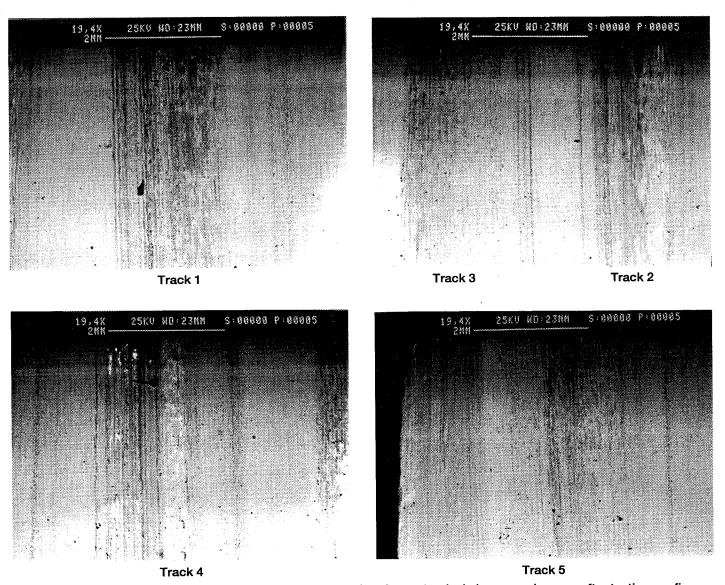


Figure 21.—Scanning electron microscope (SEM) photographs of wear tracks in low-speed runner after testing configurations 1 to 7.

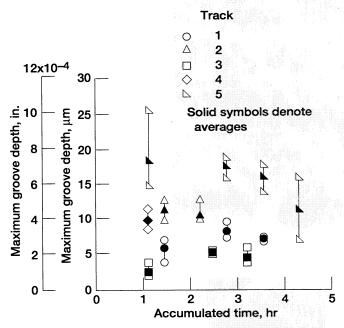


Figure 24.—Maximum, minimum, and average groove depth of brush seal wear tracks on low-speed runner after testing configurations 1 to 8 in LN₂ as function of accumulated time of shaft rotation.

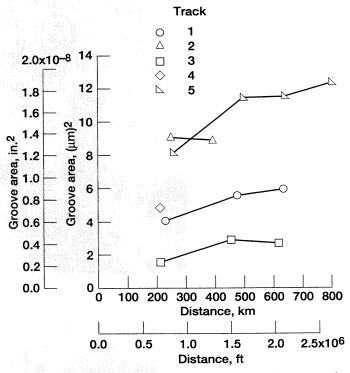


Figure 25.—Average groove area of brush seal wear tracks after testing configurations 1 to 8 in LN₂ as function of rotation distance.

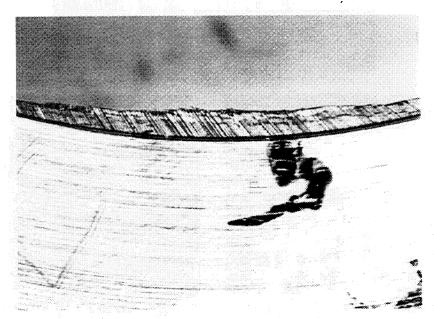


Figure 26.—Posttest brush seal showing unevenness of bristles.

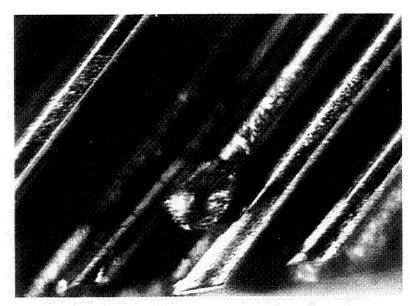
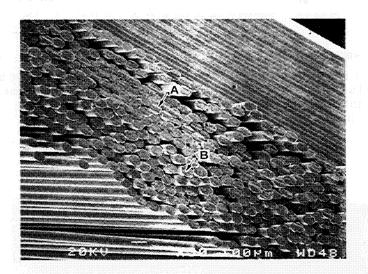


Figure 27.—Melted bristle tip.



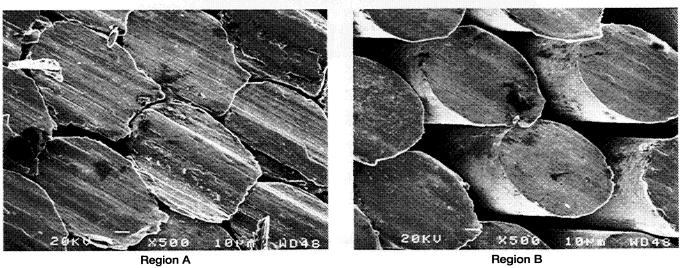


Figure 28.—Bristle wear in LN₂ tests; substantial wear shown on downstream bristles (region A) which were closer to back washer.

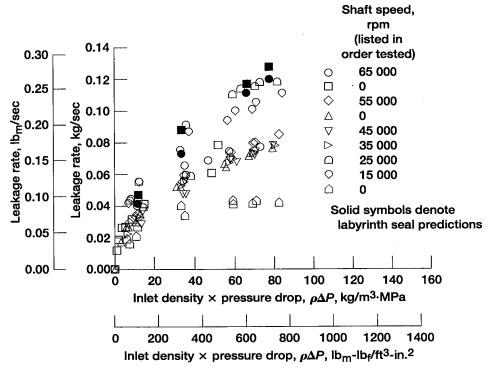


Figure 29.—Comparison of LH $_2$ leakage performance of single brush seal at various speeds and leakage predictions for 12-tooth, 0.127- μ m- (0.005-in.-) radial-clearance labyrinth seal at 0 and 65 000 rpm as function of inlet density times pressure drop across seal for configuration 9.

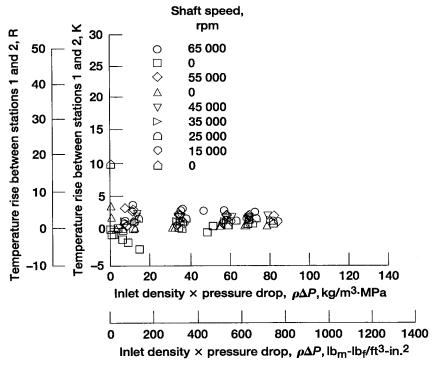


Figure 30.—Temperature rise across single brush seal in LH_2 as function of inlet density times pressure drop across seal for configuration 9 at all shaft speeds.

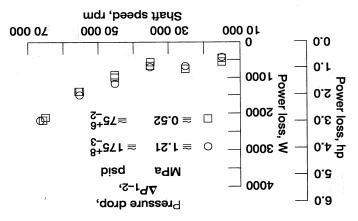


Figure 31.—Power loss to fluid across brush seal in LH₂ as function of shaft speed for pressure drops across seal of 0.52 and 1.21 MPa (75 and 175 paid). Power loss is \dot{m} ($h_2 - h_1$) in watts ($h_2 = (778/550)\dot{m}(h_2 - h_1)$) where \dot{m} is mass flow rate through seal, kg/sec (lb_m/sec); and h_2 and h_1 are the fluid enthalpy at stations 1 and 2, J/kg (Btu/lb).

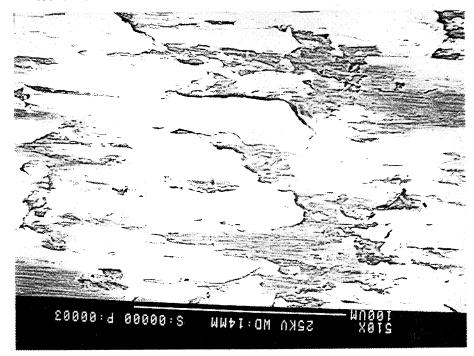


Figure 32.—Bristle material transferred to seal runner after testing in LH $_{\!\!\! 2.}$ Configuration 9. Magnification 510.

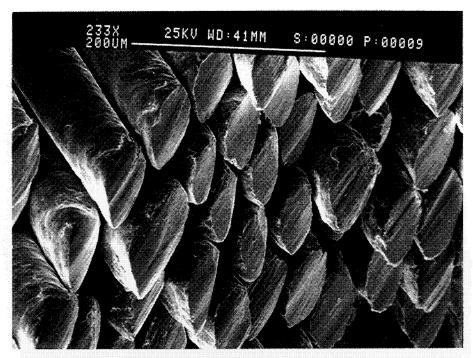


Figure 33.—Smearing type wear of Haynes-25 bristle tips after testing in LH₂. Configuration 9. Magnification 233.

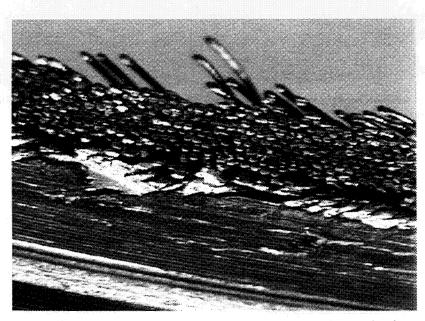


Figure 34.—Outer bristles of brush seal bent axially after testing in LH₂. Configuration 9.

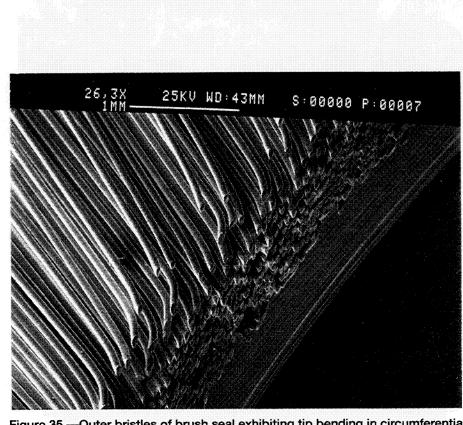


Figure 35.—Outer bristles of brush seal exhibiting tip bending in circumferential direction after testing in LH_2 . Configuration 9.

Appendix A

Instrument Description List

Chan. No.	No.	Name		Location/Description
			0-3000 PSIG	GH2 SUPPLY PRESSURE FROM TUBE TRAILER AT CELL
1		GHIN	0-3000 PSIG	GH2 PRESSURE UPSTREAM OF MAIN SUPPLY REGULATOR FH269 IN CELL
2 3		GHMNVN	0-2000 PSIG	GH2 MAIN SUPPLY LINE VENTURI PRESSURE
		GHMVDP	0-50 PSID	GH2 MAIN SUPPLY LINE VENTURI DELTA P
4			0-2000 PSIG	GH2 TURBINE SUPPLY LINE VENTURI PRESSURE
5		GHTBVN	0-100 PSID	GH2 TURBINE SUPPLY LINE DELTA: P
6		GHTVDP		GH2 TURBINE SUPPLY LINE REGULATOR OUTLET PRESSURE
7			0-2000 PSIG	GH2 TURBINE INLET PRESSURE AT RIG
8		GHTBIN	0-2000 PSIG	GH2 TORDINE INDET PRESSURE AT RIG GH2 BALANCE PISTON TURBINE SIDE VENTURI PRESSURE
9		GHBTVN	0-2000 PSIG	GH2 BALANCE PISION TURBINE SIDE VENTURI DELTA P
10		GHBTDP	0-50 PSID	GH2 BALANCE PISTON TURBINE SIDE VENTORY DEBTA F
11			0-2000 PSIG	GH2 BALANCE PISTON SEAL SIDE VENTURI PRESSURE
12		GHBSVN	0-2000 PSIG	GH2 BALANCE PISTON SEAL SIDE VENTURI DELTA P
13		GHBSDP	0-10 PSID 0-2000 PSIG	GH2 BALANCE PISTON SEAL SIDE INLET PRESSURE AT RIG
14				GH2 TURBINE NOZZLE INLET PRESSURE
15		GHTNIN	0-1000 PSIG	GH2 TURBINE NOZZLE OUTLET CAVITY PRESSURE
16		GHTNOC	0-1000 PSIG	GH2 TURBINE ROTOR OUTLET CAVITY PRESSURE
17		GHROUT	0-1000 PSIG 0-1000 PSIG	GH2 TURBINE OUTLET TORUS PRESSURE
18			0-1000 PSIG	GH2 TURBINE NOZZLE OUTLET TIP PRESSURE
19		GHTNOT	0-1000 PSIG	GH2 TURBINE NOZZLE OUTLET HUB PRESSURE
20		GHTNOH	0-1000 PSIG	GH2 TURBINE ROTOR OUTLET TIP PRESSURE
21		GHROT	0-1000 PSIG	GH2 TURBINE ROTOR OUTLET HUB PRESSURE
22		GHROH	0-1000 PSIG	GH2 TURBINE OUTLET LINE PRESSURE 1
23		GHTO1	0-1000 PSIG	GH2 TURBINE OUTLET LINE PRESSURE 2
24		GHTO2	0-2000 PSIG	GH2 BALBANCE PISTON OUTLET LINE PRESSURE
25		GHBPO	0-3000 PSIG	LH2 TANK H-50 PRESSURE
26		PRTANK	0-2000 PSIG	LH2 MAIN SUPPLY LINE VENTURI PRESSURE
27		LHMNVN	0-300 PSID	LH2 MAIN SUPPLY LINE VENTURI DELTA P
28		LHMVDP LHTBVN	0-300 PSID 0-2000 PSIG	LH2 TURBINE SIDE BEARING SUPPLY LINE VENTURI PRESSURE
29		LHTBDP	0-100 PSID	LH2 TURBINE SIDE BEARING SUPPLY LINE VENTURI DELTA P
30 31		LHSBVN	0-2000 PSIG	LH2 SEAL SIDE BEARING SUPPLY LINE VENTURI PRESSURE
32		LHSBDP	0-2000 F51G	LH2 SEAL SIDE BEARING SUPPLY LINE VENTURI DELTA P
32		LHSIVN	0-2000 PSIG	LH2 BRUSH SEAL INLET LINE VENTURI PRESSURE
34		LHSIDP	0-100 PSID	LH2 BRUSH SEAL INLET LINE VENTURI DELTA P
35		LHTBI	0-2000 PSIG	LH2 TURBINE SIDE BEARING SUPPLY LINE INLET PRESSURE AT RIG
36		LHSBI	0-2000 PSIG	LH2 SEAL SIDE BEARING SUPPLY LINE INLET PRESSURE AT RIG
37		LHSI	0-2000 PSIG	LH2 BRUSH SEAL INLET LINE PRESSURE AT RIG
38		LHSBYI	0-2000 PSIG	LH2 BRUSH SEAL CHILL DOWN BYPASS LINE INLET PRESSURE
39				
40		LHTBO	0-1000 PSIG	LH2 TURBINE SIDE BEARING OUTLET LINE PRESSURE
41		LHSBO	0-2000 PSIG	LH2 SEAL SIDE BEARING OUTLET LINE PRESSURE
42		LHSO	0-2000 PSIG	LH2 BRUSH SEAL OUTLET LINE PRESSURE
43		LHSLV1	0-2000 PSIG	LH2 BRUSH SEAL LEAKAGE OUTLET LINE VENTURI PRESSURE 1
44		LHSDP1	0-10 PSID	LH2 BRUSH SEAL LEAKAGE OUTLET LINE VENTURI DELTA P 1
4.5		LHSLV2	0-2000 PSIG	LH2 BRUSH SEAL LEAKAGE OUTLET LINE VENTURI PRESSURE 2
46		LHSDP2	0-5 PSID	LH2 BRUSH SEAL LEAKAGE OUTLET LINE VENTURI DELTA P 2
47				
48		GHTOTT	360-600 R	GH2 TURBINE OUTLET TORUS TOEMPERATURE
49		GHBPOT	100-600 R	GH2 BALANCE PISTON OUTLET LINE TEMPERATURE
50		GHMVT	360-600 R	GH2 MAIN SUPPLY LINE VENTURI TEMPERATURE
51		GHTVT	360-600 R	GH2 TURBINE SUPPLY LINE VENTURI TEMPERATURE
52		GHTIT	360-600 R	GH2 TURBINE SUPPLY LINE INLET TEMPERATURE AT RIG
53		GHBTVT	360-600 R	GH2 BALANCE PISTON TURBINE SIDE VENTURI TEMPERATURE
54		GHBSVT	360-600 R	GH2 BALANCE PISTON SEAL SIDE VENTURI TEMPERATURE

Escor Chan. No.	FM-tape Chan. No.		Expected Engineering Units Range	Location/Description
55		GHTOT1	100-600 R	GH2 TURBINE OUTLET LINE TEMPERATURE 1
56		GHTOT2	100-600 R	GH2 TURBINE OUTLET LINE TEMPERATURE 2
57		LHMVT	36-600 R	LH2 MAIN SUPPLY LINE VENTURI TEMPERATURE
58		LHTBVT	36-600 R	LH2 TURBINE SIDE BEARING SUPPLY LINE VENTURI TEMPERATURE
59		LHSBVT	36-600 R	LH2 SEAL SIDE BEARING SUPPLY LINE VENTURI TEMPERATURE
60		LHSIVT	36-600 R	LH2 BRUSH SEAL INLET LINE VENTURI TEMPERATURE
61		LHTBIT	36-600 R	LH2 TURBINE SIDE BEARING SUPPLY LINE INLET TEMPERATURE AT RIG
62		LHSBIT	36-600 R	LH2 SEAL SIDE BEARING SUPPLY LINE INLET TEMPERATURE AT RIG
63		LHSIT	36-600 R	LH2 BRUSH SEAL INLET LINE TEMPERATURE AT RIG
64		LHSBYT	36-600 R	LH2 BRUSH SEAL CHILLDOWN LINE INLET TEMPERATURE AT RIG
65		TIMBOM	26 600 B	LH2 TURBINE SIDE BEARING OUTLET LINE TEMPERATURE AT RIG
66		LHTBOT	36-600 R	(REDUNDANT THERMOCOUPLE USED FOR ABORT)
67		LHSBOT	36-600 R	LH2 SEAL SIDE BEARING OUTLET LINE TEMPERATURE AT RIG (REDUNDANT THERMOCOUPLE USED FOR ABORT)
68		LHSOT	36-600 R	LH2 BRUSH SEAL OUTLET LINE TEMPERATURE AT RIG
69		LHSLT1	36-700 R	LH2 BRUSH SEAL LEAKAGE OUTLET LINE VENTURI TEMPERATURE 1
70		LHSLT2	36-700 R	LH2 BRUSH SEAL LEAKAGE OUTLET LINE VENTURI TEMPERATURE 2
71			36-600 R	SHORTED INPUT TO INDICATE REFERENCE TEMPERATURE
72		PST1A	0-2000 PSIG	PRESSURE AT STATION 1 - 11 DEG., 15 MIN.
73		PST1B	0-2000 PSIG	PRESSURE AT STATION 1 - 101 DEG., 15 MIN.
74		PST1C	0-2000 PSIG	PRESSURE AT STATION 1 - 191 DEG., 15 MIN. PRESSURE AT STATION 1 - 281 DEG., 15 MIN.
75 76		PST1D PST2E	0-2000 PSIG 0-2000 PSIG	PRESSURE AT STATION 2 - 45 DEG.
77		PST2F	0-2000 PSIG	PRESSURE AT STATION 2 - 225 DEG.
78		PST3G	0-2000 PSIG	PRESSURE AT STATION 3 - 90 DEG.
76 79		PST3H	0-2000 PSIG	PRESSURE AT STATION 3 - 270 DEG.
80		PST4A	0-2000 PSIG	PRESSURE AT STATION 4 - 11 DEG., 15 MIN.
81		PST4C	0-2000 PSIG	PRESSURE AT STATION 4 - 191 DEG., 15 MIN.
82		PST5A	0-2000 PSIG	PRESSURE AT STATION 5 - 11 DEG., 15 MIN.
83		PST5B	0-2000 PSIG	PRESSURE AT STATION 5 - 101 DEG., 15 MIN.
84		PST5C	0-2000 PSIG	PRESSURE AT STATION 5 - 191 DEG., 15 MIN.
85		PST5D	0-2000 PSIG	PRESSURE AT STATION 5 - 281 DEG., 15 MIN.
86		TST1A	36-800 R	TEMPERATURE AT STATION 1 - 78 DEG., 45 MIN.
87		TST1B	36-800 R	TEMPERATURE AT STATION 1 - 168 DEG., 45 MIN.
88		TST1C	36-800 R	TEMPERATURE AT STATION 1 - 258 DEG., 45 MIN.
89		TST1D	36-800 R	TEMPERATURE AT STATION 1 - 348 DEG., 45 MIN.
90		TST2E	36-800 R	TEMPERATURE AT STATION 2 - 135 DEG.
91		TST2F	36-800 R	TEMPERATURE AT STATION 2 - 315 DEG.
92		TST3G	36-800 R	TEMPERATURE AT STATION 3 - 0 DEG.
93		TST3H	36-800 R	TEMPERATURE AT STATION 3 - 180 DEG.
94		TST4A	36-800 R	TEMPERATURE AT STATION 4 - 78 DEG., 45 MIN.
95		TST4C	36-800 R 36-800 R	TEMPERATURE AT STATION 4 - 258 DEG., 45 MIN. TEMPERATURE AT STATION 5 - 78 DEG., 45 MIN.
96 97		TST5A TST5B	36-800 R	TEMPERATURE AT STATION 5 - 168 DEG., 45 MIN.
98		TST5C	36-800 R	TEMPERATURE AT STATION 5 - 258 DEG., 45 MIN.
99		TST5D	36-800 R	TEMPERATURE AT STATION 5 - 348 DEG., 45 MIN.
100	2	SP1	0-50000 RPM	SPEED PICKUP OFF OF BALANCE PISTON 1
101	3	SP2	0-50000 RPM	SPEED PICKUP OFF OF BALANCE PISTON 2
102	-	GHMNFL	0-0.3 LB/S	GH2 FLOW THROUGH MAIN SUPPLY LINE VENTURI (CALC.)
103		GHTFL	0-0.1 LB/S	GH2 FLOW THROUGH TURBINE SUPPLY LINE VENTURI (CALC.)
104		GHBTFL	0-0.2 LB/S	GH2 FLOW THROUGH BALANCE PISTON TURBINE SIDE SUPPLY VENTURI (CALC.)
105		GHBSFL	0-0.2 LB/S	GH2 FLOW THROUGH BALANCE PISTON SEAL SIDE SUPPLY LINE VENTURI (CALC.)
106		LHMNFL	0-0.5 LB/S	LH2 FLOW THROUGH MAIN SUPPLY LINE VENTURI (CALC.)

Escor Chan.	FM-tape Chan.		Expected Engineering	
No.		Name		Location/Description
107		LHTBFL		LH2 FLOW THROUGH TURBINE SIDE BEARING SUPPLY LINE VENTURI (CALC.)
108		LHSBFL		LH2 FLOW THROUGH SEAL SIDE BEARING SUPPLY LINE VENTURI (CALC.)
109		LHSFL	0-0.45 LB/S	LH2 FLOW THROUGH BRUSH SEAL SUPPLY LINE VENTURI (CALC.)
110		LHSLF1	0-0.2 LB/S	LH2 FLOW THROUGH BRUSH SEAL LEAKAGE LINE VENTURI 1 (CALC.)
111		LHSLF2	0-0.2 LB/S	LH2 FLOW THROUGH BRUSH SEAL LEAKAGE LINE VENTURI 2 (CALC.)
		TESC. 1	0-2400 PSIG	TESCOM REGULATOR PRESSURE FOR VALVE 269
		TESC.2	0-2400 PSIG	TESCOM REGULATOR PREESURE FOR VALVE 275
		DELTA S	0-1000 PSID	SEAL PISTON DELTA P - DIFFERENCE BETWEEN CH 72 AND CH 82
		DELTA B	0-1000 PSID	BALANCE PISTON DELTA P - DIFFERENCE BETWEEN CH 14 AND CH 11
		HYDPP	0-5000 PSIG	HYDRAULIC PUMP PRESSURE
		HYDPT	TYPE T	HYDRAULIC PUMP TEMPERATURE
	9	B #4	10-60 MIL	40 DEGREE SEAL END PROXIMITY PROBE
	10	B #5	10-60 MIL	130 DEGREE SEAL END PROXIMITY PROBE
	11	B #6	10-60 MIL	220 DEGREE SEAL END PROXIMITY PROBE
		H-27 P	0-30 PSIG	H-27 TRAILER PRESSURE
		H2 P	0-2400 PSIG	H2 TUBE TRAILER PRESSURE
	1	BPAPP	15-80 MIL	BALANCE PISTON AXIAL PROXIMITY PROBE
	5	ZDRASE	0-20 G	ZERO DEGREE RADIAL SEAL END ACCELERATION
	14	IRIG-B		TIME CODE SIGNAL

Note: Some instrumentation ranges were changed for specific configurations.

Appendix B

Uncertainty Analysis

An uncertainty analysis was performed to determine the potential error in key experimental parameters: seal leakage rate, mean pressure at each station, and pressure drop across the seal. The procedure used to determine the uncertainty in the experimental results follows that described by Davidian, Dieck, and Chuang (ref. 23).

The total uncertainty of a measurement is caused by a random (precision) error and a fixed, or systematic (bias), error. The sources of error can be divided into three categories: calibration, data acquisition, and data reduction. No bias errors, however, were included in the analysis because the setup procedure (i.e., electronic calibration) was considered sufficient to make such errors negligible. Furthermore, data reduction errors were assumed to be small. Consequently, only precision errors due to instrumentation calibration and data acquisition were considered.

The precision of the reported leakage rate is a function of several measured parameters because the measurement was obtained using a venturi meter. The flow equation used to calculate the leakage rate m is

$$m = \frac{1}{4} \frac{c_{\nu} \pi d_2^2}{\sqrt{1 - \left(\frac{d_2}{d_1}\right)^4}} \sqrt{2\rho \Delta p}$$
 (A1)

where c_{ν} is the venturi flow coefficient; d_2 is the throat diameter; d_1 is the main tube diameter; ρ is the density; Δp is the pressure drop across the venturi. By inspecting equation (A1), the precision index, which propagates the errors occurring in measured parameters to the calculated parameter through the use of influence coefficients, can be defined as

$$S_{m} = \left[\left(\frac{\partial m}{\partial d_{1}} S_{d_{1}} \right)^{2} + \left(\frac{\partial m}{\partial d_{2}} S_{d_{2}} \right)^{2} + \left(\frac{\partial m}{\partial \Delta p} S_{\Delta p} \right)^{2} + \left(\frac{\partial m}{\partial P} S_{P} \right)^{2} + \left(\frac{\partial m}{\partial T} S_{T} \right)^{2} \right]^{1/2}$$
(A2)

where S_m is the precision index. The primary measurements are the main tube diameter d_1 , throat diameter d_2 , pressure drop across the venturi Δp , static pressure P, and temperature T. Static pressure and temperature are introduced because density

was determined from these two properties and not measured directly. The associated influence coefficients can be determined by differentiating the flow equation with respect to the primary parameters:

$$\frac{\partial m}{\partial d_1} = -\frac{c_\nu \pi d_2^6}{2d_1^5} \sqrt{2\rho \Delta p} \left[1 - \left(\frac{d_2}{d_1} \right)^4 \right]^{-3/2} \tag{A3}$$

$$\frac{\partial m}{\partial d_2} = \frac{c_v \pi d_2}{2} \sqrt{2\rho \Delta p} \left[1 - \left(\frac{d_2}{d_1} \right)^4 \right]^{-3/2} \tag{A4}$$

$$\frac{\partial m}{\partial \Delta p} = \frac{1}{4} \frac{c_{\nu} \pi d_2^2 \rho}{\sqrt{2\rho \Delta p}} \left[1 - \left(\frac{d_2}{d_1} \right)^4 \right]^{-1/2} \tag{A5}$$

$$\frac{\partial m}{\partial \rho} = \frac{1}{4} \frac{c_{\nu} \pi d_2^2 \Delta p}{\sqrt{2\rho \Delta p}} \left[1 - \left(\frac{d_2}{d_1} \right)^4 \right]^{-1/2}$$
 (A6)

Two additional influence coefficients are required to relate density to static pressure and temperature. Simple chain rule provides these relationships:

$$\frac{\partial m}{\partial P} = \frac{\partial m}{\partial \rho} \frac{\partial \rho}{\partial P} \tag{A7}$$

$$\frac{\partial m}{\partial T} = \frac{\partial m}{\partial \rho} \frac{\partial \rho}{\partial T} \tag{A8}$$

Using a fluids properties program called GASP (ref. 24), the partials $\partial \rho/\partial P$ and $\partial \rho/\partial T$ were obtained by perturbing the input pressure and temperature and observing the effect on density.

Following the procedure described by Davidian (ref. 23), the uncertainty U is then determined by applying Student's t value t_{95} to the precision index S_m to assign a confidence level to the numerical value. The relationship

$$U_{99} = t_{95} * S_m \tag{A9}$$

was used to approximate 99 percent coverage.

TABLE IV.—UNCERTAINTY OF EXPERIMENTAL LEAKAGE RATE FOR SEAL CONFIGURATIONS

Seal	Config- uration	Leakage ra	ate precision,
:		Venturi 1	Venturi 2
Labyrinth Brush	1 2 3 4 5 6 7 8	10.5 to 1.0 12.0 to 2.7 140 to 2.7 117 to 2.7 78.5 to 3.5 95 to 5.8 3.2 to 2.8 2.7 to 2.7 3.5 to 3.3	3.4 to 1.0 10.2 to 2.1 2.3 to 2.1 3.6 to 2.1 3.5 to 2.1 3.3 to 2.1 3.0 to 2.2 2.1 to 2.1 3.4 to 3.1

TABLE V.—AVERAGE PRESSURE MEASUREMENT UNCERTAINTY AT EACH STATION

Station	measi	e pressure urement rtainty
	MPa	psi
1	0.008	1.1
2	.043	6.2
3	.026	3.8
4	.068	9.8
5	.011	1.6

TABLE VI.—MEASUREMENT UNCERTAINTY OF PRES-SURE DROP BETWEEN STATIONS

Stations		rement ainty of re drop
	MPa	psi
1 to 2	0.033	4.8
1 to 3	.028	4.1
1 to 5	.014	2.1
2 to 4	.046	6.7
2 to 5	.030	4.4
4 to 5	.047	6.8

The uncertainty of the experimental leakage rate for the seal configurations are presented as a percent of the measured value in table IV. Uncertainty varied for each seal configuration because of the changes in the hardware used to measure leakage rates. Venturi meters and the differential pressure transducers were changed during the test program to better match the leakage characteristics of the particular seal being tested. The intent was to minimize uncertainty in the results. Furthermore, a pair of venturi meters, located in series and downstream of the test seal, were used to provide redundancy. The table includes the uncertainty for each venturi measurement. In addition, a range of uncertainty is given for each case. The uncertainty at low- and high-pressure drops across the seal is reported. Although most of the cases showed small variation, venturi meter 1 for seal configurations 3 through 6 incurred high uncertainty because of the differential pressure transducer used to measure the pressure gradient across the venturi meter. The transducer had a high nonlinearity error associated with it. It was replaced for later tests.

The uncertainty of the mean pressure at each station, which was the average of four or two separate pressure transducers located at different positions around the circumference of the seal, were also determined and are displayed in table V. The uncertainty of the measured pressure drop across the seal is also important. The pressure drop was the difference between the average of two sets of pressure transducers; each set was located at different axial stations. Table VI presents the uncertainty of the measured pressure difference between each station. Although most of the leakage rate data are plotted against the pressure drop measured between stations 1 and 5, some data are not. Thus, the uncertainty in the pressure difference measurement between each station is provided to be complete. In general, the uncertainty of the measured mean and differential pressures is reasonable.

Appendix

SI Units Data Tables-

BAROMETER: 98.839 kPa CELL2 CC TEST FACILITY: CRYOGENIC APPLICATIONS SEALS FOR BRUSH RESEARCH PROGRAM:

DELTA-F STA 1-5 (MPd) 0.000 0.110 0.1110 0.1182 0.1182 0.1182 0.1183 0.1183 0.01 AVERAGE LEAKAGE RATE (Kg/S) AVERAGE SHAFT SPEED (REV/S) AVG TEMP STATION 5 991.48 888.33.57 Ξ in position -AVG TEMP STATION 1 88.19 883.70 883 Ξ Single brush AVG PRESS STATION 5 (MPa) AVG PRESS STATION 1 N (MPa) CONFIGURATION NO. FLUID: NITROGEN RDG AVG SCANS A NO COLOR SE SECONO COLOR SE SE 11226 12226

BAROMETER: 98.839 KPa

Single brush in position 1 2 CONFIGURATION NO.

DELTA-P STA 1-5 (MPd)	0.000000000000000000000000000000000000
AVERAGE LEAKAGE RATE (Kg/S)	0.000000000000000000000000000000000000
AVERAGE SHAFT SPEED (REV/S)	0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-
AVG TEMP STATION 5 (K)	100 102.33 105.53 102.33 888.888888888888.03 103.03
AVG TEMP STATION 1 (K)	99.09 1022.24
AVG PRESS STATION 5 (MPa)	44.0.0.0.0.444444.0.0.0.40.0.0.444444.0.0.044444.0.0.0444444
N AVG PRESS STATION 1 (MPa)	ចុះចុះចុះចុះចុះចុះចុះចុះចុះចុះចុះចុះចុះច
FLUID: NITROGEN RDG AVG SCANS A	139 ALL SCNS 188 ALL SCNS 189 ALL SCNS 188 ALL SCNS 188 ALL SCNS 188 ALL SCNS 189 ALL SCNS 199 ALL SCNS 199 ALL SCNS 209 ALL SCNS 200 A

CONFIGURATION NO. $\,\,3\,\,$ 2 Brushes far apart at stations 2 & 5

288 ALL SCNS 289 ALL SCNS 290 ALL SCNS 291 ALL SCNS 292 ALL SCNS	PAR	AL P	PAR	A P	ALL	A A E	<u> </u>	A A	<u> </u>	₽.P.	AA	ALL	ALL	ALL	ALL	AL	E E	AL A	E P	<u> </u>	AL;		<u> </u>	22		FLUID: NITROGEN RDG AVG SCANS
មាល់ក្នុងក្នុង ភូទ្ធិស្វិស្សិស្សិស្សិស្សិស្សិស្សិស្សិស្សិស្ស	ເພດຄ	ကကျ	ກຸບາບ	າຫຸຕ	igigi W W	တတ	ກຫ	တက	. m : s	(11 (11		1010	an ar	i di di	יטיטי	טוטו	າຫາ	າຫາ	, , ,	ກຸບາເ	ט ויט ויכ	الناد	ກຸດເ	וטונ	(MPa)	AVG PRESS STATION 1
		5.16	1	im	$\dot{\sim}$	ia							5.38	5.37	55. 25. 25. 25. 25. 25. 25. 25. 25. 25.		5.04	4.93	4.00	4.86	4.97	7.5 0.00	55. 150. 150.	5.36 30	(MPa)	AVG PRESS STATION 3
	5.30 39	5.03 5.17	4.78 4.91	4.76 4.76	5.14 5.01	5.30										\	منحد	منمنہ	'n	200	oio i	<u></u>	5.23 16	سأس	(MPa)	AVG PRESS STATION 4
5.10 4.74 4.39 4.04 3.68	5.38	4.52	4.19	3.83 3.63	4.86 4.51	5.38	4. 88	4.18 4.53	ა.ა. ა.ა.გ	3.67 3.47	3.84 3.84	4.51	.5.5 22.5 22.5 23.5 25.5 25.5 25.5 25.5	5.26	5.04 04.8	4.70	4.35	4.01	3.65 65	3.4. 830	4.34	4.70 4.52	5.03 4.86	5.34	(MPa)	AVG PRESS STATION 5
83.63 83.63 83.73 83.75	89.28 83.88	84.83 85.72	84.00 84.14	83.75 83.75	83.48 83.66	84.20 83.59	83.42 83.48	83.35 83.52	83.26 83.36	83.02	82.86	82.84 02.82	82.86	82.74	82.77 82.77	82.76	82.80 08.38	82.86 74	82.89 73	82.62 82.75	83.05 82.94	83.09 82.94	82.99 82.95	83.11 83.13	<u>*</u>	AVG TEMP STATION 1
85.73 85.51 85.11 85.11	94.13 93.63	85.32 86.24	84.47 84.57	84.28 84.33	84.24 84.26	106.06 84.92	84.07 85.38	83.86 84.13	83.87 84.00	83.68	83.53	83.72 83.72	8.03	280	83.42	383	83. 33. 35. 35.	83.46	83.47	83.29 34.29	88. 55.	83.69 83.58	83.76 83.70	85.36 84.09	8	AVG TEMP STATION 3
85.61 85.15 85.02	95.89 93.53	85.18 86.05	84.33 84.57	84.11 84.17	84.06	106.23 84.33	83.92 85.27	83.73 83.94	83.79 83.80	83.54	83.37	83.60 83.60	87.87 87.87	83.72	88.01	383	385 1991	83.15 26.15	83.25	83.04 83.12	83.34 83.25	83.36 83.27	83.23 83.26	84.33 83.55	?	AVG TEMP STATION 4
94. 244 90. 840 89. 775 88. 875 88. 678	104.062	87.775 88.662	87.118 87.160	86.824	87.295 86.931	101.822 89.174	86.932 89.239	86.434 86.728	86.514 86.562	86.593	86.354	86.877 86.877	93.886	90.163	86.513	86.408	86.452	86.487	86.777	86.470 86.547	86.514 86.474	86.399 86.330	86.402 86.416	89.815 87.221	Ê	AVG TEMP
246.8 250.9 5 250.9 249.8 249.8	25.0	-6-6		565	9-1-	. 8 0 U	8 8 4 4	883 843	83	2000	000	0000	a & .	065	56	56	50		50	<u>-</u> -	6 6	9 . 9		99	(REV/S)	AVERAGE SHAFT
0.05																									(Kg/S)	AVERAGE LEAKAGE

FLUID: NITROGEN

AVERAGE LEAKAGE DATE	_			
AVERAGE SHAFT Speen	(REV/S)			
AVG TEMP STATION 5	(K)	88.617 88.816 99.035 90.489 90.489 97.375 116.825 86.738 87.179 86.174 86.295 86.205 8	117.054 117.054 144.767 189.037 88.060 87.335 86.850 86.850 86.127 86.127 86.127 87.258 1122.324 116.128 110.128	115.205 1115.205 1118.205 1118.573 1131.803 1131.555 190.051 88.051 86.661 87.067 88.554 86.661 87.067 101.744
AVG TEMP STATION 4	(X	88.38.38.39.39.39.39.39.39.39.39.39.39.39.39.39.	101.08 84.35 84.35 84.16 84.16 84.16 84.22 83.72 83.72 100.68 99.58 99.58 99.58	995.77 100.99 1115.04 1113.28 1193.28 84.58 84.54 84.92 86.98 86.98 86.98 94.70
AVG TEMP STATION 3	(K)	85.93 85.93 85.93 85.93 85.93 85.93 86 86 86 86 86 86 86 86 86 86 86 86 86	1011 1451.76 1451.76 1451.76 184.31 184.10 116.93 1004.44 1004.44 1004.44 1004.44 1004.44 1004.44	99999999999999999999999999999999999999
AVG TEMP STATION 1	3	88888888888888888888888888888888888888	88.888.888.888.888.89.98.72.09.888.89.99.72.09.888.89.99.988.39.70.72.09.888.99.98.89.70.72.09.888.99.98.70.70.70.70.70.70.70.70.70.70.70.70.70.	99.99 90.09 90.09 90.09 84.51 84.51 85.10 90.034 90.034
AVG PRESS STATION 5	(MPa)	444°°°°°°°°°°444°°°°°°°°°°°°°°°°°°°°°	v.v.v.v.v.4.4.4.4.4.v.v.v.v.v.4.4.4.v. 0.4.0.4.4.4.4.4.4.v.v.v.v.v.4.4.4.v.v. 0.4.0.4.4.4.4.4.4.4.4.4.4.4.4.4.4.4.4.	.4446.6.0.0.0.444.6.6.6.44.6.6.6.6.6.6.6
AVG PRESS STATION 4	(MPa)	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	ჀჀჀჀჀჀჀჀჀჀ ႯჅჅჇჇႼႼჅჅჅჅ ႨႼჅჅჅჅჅჅჅჅჅ	დდდდდდდდდდ 4.000.000 8.118.4 6.000.000.000.000.000.000.000.000.000.0
AVG PRESS STATION 3	(MPa)		ក្រសួលក្រហូកក្រសួល ក្រសួលក្រសួលក្រសួលក្រសួលក្រសួលក្រសួលក្រសួលក្រសួលក្រសួលក្រសួលក្រសួលក្រសួលក្រសួលក្រសួលក្រសួលក្រ	გარიტიტიტიტი 1000012000 1000012000
VG PRESS	(MPa)			
FLUID: NITROGEN RDG AVG SCANS A		293 ALL 294 ALL 295 ALL 295 ALL 295 ALL 297 ALL 298 ALL 208 AL	SCOCOO SC	

DELTA-P STA 1-2 (MPd) DELTA-P STA 1-5 (MPd) 0.053 0.089 0.089 0.0124 0.0126 0.0127 0.0128 0.012 AVERAGE SHAFT SPEED (REV/S) 2 AVG TEMP STATION 5 992.21 991.653 991.653 990.654 990.657 990.657 991.373 AVG TEMP STATION 2 ంర 884.98 883.98 88 ന .. positions ---AVG TEMP STATION 1 tightly packed AVG PRESS STATION 5 (MPa) AVG PRESS STATION 2 Brushes (MPa) N AVG PRESS STATION 1 4 (MPa) CONFIGURATION NO. FLUID: NITROGEN RDG AVG SCANS

CONFIGURATION NO. RESEARCH PROGRAM: BRUSH SEALS FOR CRYOGENIC APPLICATIONS TEST FACILITY: CCL - CELL2 2 Brushes tightly packed .. positions 3 & 4 BAROMETER: 99.280 kPa

4

416 ALL SCNS 417 ALL SCNS 418 ALL SCNS 421 ALL SCNS 422 ALL SCNS 423 ALL SCNS 423 ALL SCNS 424 ALL SCNS 425 ALL SCNS 435 ALL SCNS 436 ALL SCNS 437 ALL SCNS 438 ALL SCNS 439 ALL SCNS 439 ALL SCNS 430 ALL SCNS 431 ALL SCNS 432 ALL SCNS 433 ALL SCNS 434 ALL SCNS 445 ALL SCNS 445 ALL SCNS 456 ALL SCNS 457 ALL SCNS 458 A	FLUID: NITROGEN RDG AVG SCANS /
######################################	AVG PRESS STATION 1
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83.359 83.359	AVG TEMP STATION 1 (K)
83.87 83.76 83.76 83.76 83.76 83.76 83.77 83.77 83.77 83.77 83.77 83.77 83.77 83.83 84.10 85.04 86.99 87.86 88.50 91.36 88.50 91.50 88.50 98	AVG TEMP STATION 2 (K)
93.09 92.30 91.76 91.76 91.76 91.77 91.77 91.77 91.77 91.77 91.77 91.77 91.77 91.77 92.17 91.85 92.56 84.22 84.22 85.24 86.94 87.10 87.10 88.32 88	AVG TEMP STATION 5
-0.11 -0.11	AVERAGE SHAFT SPEED (REV/S)
0.025 0.025 0.025 0.050 0.050 0.073 0.0073 0.0074 0.025	AVERAGE LEAKAGE RATE (Kg/S)
0.16 0.16 0.17 0.17 0.17 0.17 0.17 0.17 0.17 0.17	DELTA-P STA 1-5 (MPd)
	DELTA-P STA 1-2 (MPd)

		AVERAGE LEAKAGE RATE	(Kg/S)	0.0000000000000000000000000000000000000
99.039 kPa		AVERAGE Shaft Speed	(REV/S)	22222222222222222222222222222222222222
BAROMETER: 99.0		AVG TEMP STATION 5	(X	97. 688 885. 223 885. 223 885. 233 885.
CELL2 BAR		AVG TEMP STATION 4	(ξ	29888888888888888888888888888888888888
ITY: CCL -		AVG TEMP STATION 2	<u>X</u>	88888888888888888888888888888888888888
TEST FACILITY	ĸ	AVG TEMP STATION 1	(K)	83.83.83.83.83.83.83.83.83.83.83.83.83.8
PLICATIONS	ce: pos 1,3,	AVG PRESS STATION 5	(MPa)	mmn4444 mmn4444 mmn4444 mmn4444 mmn4444 mmn4444 mmn4444 mmn44444 mmn444444 mmn44444 mmn44444 mmn44444 mmn44444 mmn44444 mmn44444 mmn44444 mmn44444 mmn444444 mmn444444 mmn444444 mmn444444 mmn4444444 mmn444444 mmn444444 <
CRYOGENIC APPL	equally spac	AVG PRESS STATION 4	(MPa)	0.0.0.0.4.4.4.4.4.4.4.4.4.4.4.4.4.4.4.4
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: BRUSH	NO. 5	AVG PRESS STATION 1	(MPa)	ສຸກັດການການການການການການການການການການການການການກ
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FLUID: NITROGEN

AVERAGE LEAKAGE DATE	(Kg/S)	00000000000000000000000000000000000000	00000000000000000000000000000000000000	9000000000000 8000000000000000000000000	0.000000000000000000000000000000000000	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
AVERAGE SHAFT SPEED	(REV/S)	222499 2244998 22449988 2244998888888888	420.7 416.9 419.2 419.0 421.4 421.4 420.6 420.6 420.6		5885.3 5885.3 5885.9 5887.4 5666.5 573.2 573.2 587.3 587.3 587.3 587.3	
AVG TEMP STATION 5	(X)	88.864 101.564 101.564 101.564 101.564 87.100 86.182 85.970 86.719 88.038 88.834 89.701 91.400 93.488 96.258	127.461 114.849 108.360 102.913 101.140 99.923 100.826 100.757	,	141.670 113.135.4 113.115.1115 111.205 101.205 100.248 112.975 112.975 113.975	888888888888
AVG TEMP STATION 4	(K)	88.98.98.98.98.98.98.98.98.98.98.98.98.9	97.87 97.87 90.91 90.91 90.33 90.33 91.30	98888888888888888888888888888888888888	127.22 906.55 98.34 92.11 92.19 99.42 99.43	88.07 83.16 83.56 83.56 83.55 83.55 90.45
AVG TEMP STATION 2	(K)	85.27 98.35 98.35 98.35 88.38 83.37 88.33 88.33 88.11 88.11 99.99 99.99 99.96 99.96	101.07 93.48 88.67 88.29 88.34 98.85 96.85	882.553 882.554 882.553 882.553 882.553 882.553 882.553 883.611	117.86 102.15 92.15 92.58 90.98 90.87 91.83 94.08	833.24 833.27 833.24 833.24 833.24 853.26 853.26
AVG TEMP STATION 1	(K)	8833.77 883.77 883.77 883.34 887.89 87.95 90.10 90.10 90.10	88888888888888888888888888888888888888	882.13 882.13 882.13 882.14 882.28 882.28 882.15 882.15	88.03 88.25 87.52 87.52 86.12 86.72 87.26 87.56	883.37 883.37 883.37 883.37 883.37 84.17
AVG PRESS STATION 5	(MPa)	44400044460044460 			24444444444444444444444444444444444444	
AVG PRESS STATION 4	(MPa)		•	0.0.0.4.4.4.4.4.0.0.0.0.0.0.0.0.0.0.0.0	,	5.17 4.452 71.33 6.14 7.14 7.14 7.05 7.05
AVG PRESS STATION 2	(MPa)	7.00.00.44.00.00.00.00.00.00.00.00.00.00.	•	, wayayayayayayayayayayayayayayayayayayay		22.22 20.02.4 20.00.0
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AVERAGE LEAKAGE RATE (Kg/S) AVERAGE SHAFT SPEED (REV/S) 89. 649
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CONFIGURATION NO. 7 3 Brushes equally spaced - positions 1,3,5

FLUID: NITROGEN RDG AVG SCANS		662 ALL SCNS 663 ALL SCNS 664 ALL SCNS 665 ALL SCNS 666 ALL SCNS 668 ALL SCNS			PPPPP		PARA	PPPP	PPPP	PPPP	2222	ALLA	ALL	ALLE	ALL
AVG PRESS	(MPa)		ပုံ လူ လူ လူ လူ လူ လူ လူ လူ လူ လူ လူ လူ လူ လူ လူ	5.40 5.40	5.555555 5.655555 5.655555	**************************************	မှ အလည်းသူ မှ ထို လည်းသူ မှ ထို လည်းသူ	າຫຫຫຫ ວິດ 2007 2008	######################################	55555555555555555555555555555555555555	ກຫຫຫຫ ພູພູພູພ ພູພູພູພູພູພູພູພູພູພູພູພູພູພ	ကြည်း လူတွင်း လူတွင်း	5.30 5.30 5.17	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	5.17
AVG_PRESS	a)	5.227 5.227 5.006	.5.5.5.5.5.5.5.5.5.5.5.5.5.5.5.5.5.5.5	5.27 5.17 5.07 4.96 4.91	4.87 5.97 5.15 5.22	2066 2006 2006 2006 2006 2006 2006 2006	75.55.4.4.4.5 0.0000000000000000000000000	5.27 5.27	55455 5000 12000 12000	555555 5534 5664	4.88 4.88	5.14 5.22	5.21 4.92	4.79 4.83 5.00	5.13 17
AVG PRESS	a) 1	5.32 5.14 4.99 4.82 4.78 4.74	5.39 5.39 5.39	5.11 4.87 4.66 4.43 4.36	5.055 4.655	4.688 67	7.4.4.4.50 7.67 7.85	4.95 3.12 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5	4.57 4.41 4.50 4.67	55.28 5.28 10	4.93 4.75 4.43	4.69 5.06 5.28	4.87 4.87	4.53 4.58	5.09 5.18
AVG PRESS	a)	4.89 4.58 3.87 3.87	5.27 5.27 5.27	4.99 4.59 4.25 3.88	3.54 4.25 4.58	4.56 4.51	4.4.3.50 4.5537	25.00 25.00 25.00 25.00 25.00	.4.0.0.3. 4.0.0.4.0. 1.0.0.4.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.	4.55.24 4.89 4.87	2.4.5 2.4.5 2.4.5 2.4.5 2.5 2.5 2.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3	4.18 4.47 4.85	3.9.4.80 5.96	4.00 4.33 3.45 4.33	5.02
AVG TEMP	;	83.11 83.36 83.29 83.17 83.06 83.06	83.05 83.24 83.43	88.54 88.23 88.01 87.85	87.79 88.16 88.03 88.29 88.49	28888888888888888888888888888888888888	85,23 05,23	86.33 84.11 83.84	83.64 83.67 83.70	83.82 83.33 83.44	83.28 83.84 63.70	83.98 84.04 84.42	88888 84.55 88.55 88.55	33.96 33.96	84.08 84.54
TEN STEER		83.63 83.63 83.29 83.29	83.25 83.33 83.56 84.72	103.16 98.14 96.45 94.98 94.70	94.40 95.91 95.90 97.26	96.78 92.69 91.18	88.97 89.42 90.29	98.04 90.03 87.35	85.35 85.11	85.71 89.83 84.78 84.32	84.02 84.35 84.38	84.46 84.42 84.87 86.11	84.70 84.66 83.70	84.01 84.06 84.26	84.39 85.93
AVG TEMP	<u>ح</u>	84.34 83.91 83.81 83.63 83.53 83.53	83.53 84.08 87.49	110.58 105.13 101.43 98.86 98.60	97.91 99.94 100.28 107.36	102.65 95.78 93.48 92.08	90.44 91.10 91.75 92.54	103.76 92.87 88.71 87.26	85.76 85.97	85.35 84.75	84.54 84.51 84.53	84.68 84.77 85.24 86.84	85.28 84.00	84.25 84.38	84.70 89.34
AVG TEMP	:	87.839 86.372 85.767 85.493 85.239 85.233 85.198	85.276 85.558 85.112 95.111 136.872	127.016 118.638 113.938 119.740 108.778	108.011 111.113 112.219 112.653	134.032 117.678 107.088 102.681 99.741	96.279 97.279 98.588 100.354	117.342 99.938 94.095 91.581	88.562 88.944	99.700 90.700 97.942 88.415 87.124	86.493 86.281 86.485 86.372	86.657 86.869 87.499 89.394	87.201 86.947 85.814	86.264 86.264	87.097 96.594
V M	SPEED (REV/S)	0000000	700000	222222		377778	71777	22222	868888	8648		$\omega = \omega \omega$			00
AVERAGE	RATE (Kg/S)	0.07	2000000	000000000000000000000000000000000000000	0000000	00000000000000000000000000000000000000	20,000	20000 20000 20000	0.000 0.000 0.000 0.000	00000	0.065	0.07 0.07 0.03	0000 0000 0000 0000	0.0000	0.02

RESEARCH PROGRAM: BRUSH SEALS FOR CRYOGENIC APPLICATIONS TEST FACILITY: CCL - CELL2 BAROMETER: 97.653 kPa

	DELTA-P STA 1-5 (MPd)	00000000000000000000000000000000000000
	AVERAGE LEAKAGE RATE (Kg/S)	0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.
	AVERAGE SHAFT SPEED (REV/S)	00000000000000000000000000000000000000
	AVG TEMP STATION 5 (K)	88888888888888888888888888888888888888
- position	AVG TEMP STATION 1 (K)	######################################
Single Brush	AVG PRESS STATION 5 (MPa)	ででででででです。444444444444444444444444444444
	EN AVG PRESS STATION 1 (MPa)	ឨ ៹៳ឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨឨ
CONFIGURATION NO	FLUID: NITROGEN RDG SCAN	7446 7446

RESEARCH PROGRAM: BRUSH SEALS FOR CRYOGENIC APPLICATIONS TEST FACILITY: CCL - CELL2

BAROMETER: 97.653 kPa

FLUID: NITROGEN RDG SCAN	CONFIGURATION NO.
AVG PRESS STATION 1	8
AVG PRESS STATION 5	Single Brush - position
AVG TEMP STATION 1	- position 1
AVG TEMP STATION 5	
AVERAGE SHAFT	·
m	
E AVERAGE	

740 555 740 557 740 557 740 557 740 657 740 657 740 657 740 657 740 657 740 657 740 77 740 77 740 77 740 77 740 77 740 77 740 77 740 77 740 92 740 92 740 102 740 102 740 103		LUID: NITROGEN DG SCAN
おおおおおおおおおおおおおおおおおおおおおおおおおおおおおおおおおおおお	(MPa)	AVG PRESS STATION 1
22.22.22.22.22.22.22.22.22.22.22.22.22.	(MPa)	AVG PRESS STATION 5
83.27 83.27	?	AVG TEMP STATION 1
85.23 85.23 85.23 85.23 85.23 85.23 85.23 85.33	(K)	AVG TEMP STATION 5
000000000000000000000000000000000000000	(REV/S)	AVERAGE SHAFT
0.157 0.169 0.169 0.163 0.163 0.164 0.164 0.165 0.165 0.165 0.166 0.167 0.171	(Kg/S)	AVERAGE LEAKAGE
1.75 1.75 1.75 1.75 1.88 1.88 1.88 1.88 1.99 1.99 1.99 1.99	(MPd)	DELTA-P STA 1-5

RESEARCH PROGRAM: BRUSH SEALS FOR CRYOGENIC APPLICATIONS TEST FACILITY: CCL - CELL2 BAROMETER: 97.653 kPa

740 113 740 113 740 113 740 113 740 113 740 113 740 113 740 123 740 123 740 123 740 123 740 123 740 123 740 123 740 133 740 133 740 133 740 133 740 135 740 135 740 135 740 135 740 155 740 156	740 110	CONFIGURATION NO FLUID: NITROGEN RDG SCAN
Grandanananananananananananananananananan	(MPa) 5.21	NO. 8 EN AVG PRESS STATION 1
2.337 2.337 2.337 2.144 2.107	(MPa) 2.31 2.33	Single Brush AVG PRESS STATION 5
88888888888888888888888888888888888888	83.21 83.21	- position 1 AVG TEMP STATION 1
\$2.500 \$2	85.44 85.36	
666666666666666666666666666666666666666		AVERAGE SHAFT SPEED
0.190 0.190 0.196 0.197 0.198 0.198 0.199 0.199 0.199 0.199 0.199 0.199 0.199 0.200	(Kg/S) 0.185 0.195	AVERAGE LEAKAGE
	(MPd) 2.90 2.88	DELTA-P STA 1-5

DELTA-P STA 1-5 (MPd) 0.200 0.000 AVERAGE LEAKAGE RATE (Kg/S) AVERAGE SHAFT SPEED (REV/S) 5 AVG TEMP STATION $\overline{\mathfrak{S}}$ - position --AVG TEMP STATION 1 Ξ Single Brush AVG PRESS STATION 5 (MPa) AVG PRESS STATION 1 ∞ (MPa) CONFIGURATION NO. FLUID: NITROGEN / RDG SCAN / 11066 11066 11070

97.653 kPa

FACILITY: CCL - CELL2 BAROMETER: 97		AVERAGE AVERAGE DELTA-P SHAFT LEAKAGE STA 1-5 EDED		0.206 0.206
APPLICATIONS TEST FA	N NO. 8 Single Brush - position 1	AVG TEMP AVI STATION 5 SH	(K)	88888888888888888888888888888888888888
CRYOGENIC APP		AVG TEMP STATION 1	(K)	88888888888888888888888888888888888888
F0R		AVG PRESS STATION 5	(MPa)	0.000111000000000000000000000000000000
: BRUSH		GEN AVG PRESS STATION 1	(MPa)	พ.พ.พ.พ.พ.พ.พ.พ.พ.พ.พ.พ.พ.พ.พ.พ.พ.พ.พ.
RESEARCH PROGRAM	CONFIGURATION	FLUID: NITROGEN RDG SCAN A		740 259 88 251 250 270 271 272 272 272 272 272 272 272 272 272

KESEARCH PROGRAM	: BRUSH	SEALS FOR CRY	CRYOGENIC APPL	APPLICATIONS TEST	T FACILITY:	CCL - CELL2	BAROMETER:
CONFIGURATION	NO. 8	Single Brush	- position				
FLUID: NITROGEN	EN AVG PRESS STATION 1	AVG PRESS STATION 5	AVG TEMP STATION 1	AVG TEMP STATION 5	AVERAGE SHAFT SPER	AVERAGE LEAKAGE BATE	DELTA-P STA 1-5
	(MPa)	(MPa)	(K)	(X	(REV/S)	(Kg/S)	(MPd)
740 275 740 277 740 27	๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛	00000000000000011111000000000000000000	######################################	######################################		0.000000000000000000000000000000000000	44444444444444444444444444444444444444

DELTA-P STA 1-2	(MPd)	0.000111100000000000000000000000000000
DELTA-P STA 1-5	(MPd)	0.000111100000000000000000000000000000
VENTURI 2 LEAKAGE RATE	(Kg/S)	0.059 0.068 0.0077 0.0000 0.00
AVERAGE SHAFT SPEED	(REV/S)	00100000000000000000000000000000000000
AVG TEMP STATION 5	(X)	33.3.3.3.3.3.3.3.3.3.3.3.3.3.3.3.3.3.3
AVG TEMP STATION 2	€	288.588 28.599 28.588.388 28.588.388 28.588.388 28.588.388 28.5888 28.588
AVG TEMP STATION 1	3	26.99 27.28 27.28 27.28 27.28 27.28 27.28 27.28 27.28 28.39
AVG PRESS STATION 5	(MPa)	494414111114479444444444444444444444444
AVG PRESS STATION 2	(MPa)	7979-1-1-1-1999-1999-1999-1999-1999-199
AV6	(MPa)	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~
FLUID: HYDROGEN RDG AVG SCANS		S C C C C C C C C C C C C C C C C C C C
AVG		FFFFFFFFFFFFFFFFFFFFFFFFFFFFFFFFFFFFFF
FLUII		88888888888888888888888888888888888888

DELTA-P STA 1-2	(MPd)	0.000111100000000000000000000000000000
DELTA-P STA 1-5	(MPd)	0.000 0.000
VENTURI 2 LEAKAGE DATE	(Kg/S)	0.000000000000000000000000000000000000
AVERAGE SHAFT Speen	(REV/S)	28888888888888888888888888888888888888
AVG TEMP STATION 5	(K)	33.05.33.05.33.05.33.05.33.05.33.33.33.33.33.33.33.33.33.33.33.33.33
AVG TEMP STATION 2	(K)	38827272728888777272888887777778888871144163 38877777777778888777777888887777777777
AVG TEMP STATION 1	(K)	27.71.69 27.71.69 27.72.88.36.89.36.50.39.36.29.36.20.39.36.20.39.36.20.39.36.20.39.39.39.39.39.39.39.39.39.39.39.39.39.
AVG PRESS STATION 5	(MPa)	2.2.2.2.1.1.2.2.2.2.2.2.2.2.2.2.2.2.2.2
AVG PRESS STATION 2	(MPa)	2.2.2.2.1.1.2.2.2.2.2.2.2.2.2.2.2.2.2.2
AVG PRESS STATION 1	(MPa)	######################################
FLUID: HYDROGEN RDG AVG SCANS AVG PR STATIO		859 ALL SCNS 861 ALL SCNS 863 ALL SCNS 863 ALL SCNS 865 ALL SCNS 865 ALL SCNS 866 ALL SCNS 866 ALL SCNS 866 ALL SCNS 870 ALL SCNS 871 ALL SCNS 872 ALL SCNS 873 ALL SCNS 873 ALL SCNS 873 ALL SCNS 873 ALL SCNS 883 ALL SCNS 884 ALL SCNS 885 ALL SCNS 885 ALL SCNS 886 ALL SCNS 887 ALL SCNS 889 ALL SCNS 889 ALL SCNS 889 ALL SCNS 889 ALL SCNS 899 A

Appendix D

Data Tables—English Units

BAROMETER: 14.337 PSIA CELL2

BAROMETER		DELTA-P STA 1-5	(DSID)	48.39 123.89 14.89 14.89 15.10 16.10 1
CCL - CE LL2	Single brush in position 1	AVERAGE LEAKAGE RATE	(LBM/S)	0.000000000000000000000000000000000000
FACILITY:		AVERAGE SHAFT SPEED	(RPM)	10000000000000000000000000000000000000
APPLICATIONS TEST		AVG TEMP STATION 5	(<u>R</u>	1559 11359 1
CRYOGENIC APPL		AVG TEMP STATION 1	(R)	1551 1551 1551 1551 1551 1551 1551 155
PROGRAM: BRUSH SEALS FOR		AVG PRESS STATION 5	(PSIA)	782.69 755.15 660.33 660.33 660.33 660.33 660.33 656.99 656.99 616.27 738.93 738 738.93 738.93 738.93 738.93 738.9
	CONFIGURATION NO. 2	: NITROGEN AVG SCANS AVG PRESS STATION 1	(PSIA)	ALL SCNS 786.90 ALL SCNS 778.56 ALL SCNS 778.56 ALL SCNS 778.56 ALL SCNS 778.56 ALL SCNS 764.71 ALL SCNS 764.71 ALL SCNS 767.92 ALL SCNS 767.93 ALL SCNS 767.43 ALL SCNS 768.35 ALL SCNS 769.17 ALL SCNS 769.17 ALL SCNS 769.17 ALL SCNS 777.43 ALL SCNS 776.13 ALL SCNS 766.10 ALL SCNS 766.10 ALL SCNS 776.59
RESEARCH	CONFIG	FLUID: RDG A		22222222222222222222222222222222222222

BAROMETER:		DELTA-P STA 1-5	(PSID)	123. 24.45. 25.55. 26.55. 27.55.
CCL - CELL2		AVERAGE LEAKAGE	(LBM/S)	0.157 0.107
ST FACILITY:		AVERAGE SHAFT SPEED	(RPM)	255126.0 255126
ATIONS TE	in position 1	AVG TEMP STATION 5	(R)	188.70 188.70 158.74 158.54 158.54 158.54 158.54 158.55 159.64 150.68 16
CRYOGENIC APPLIO		AVG TEMP STATION 1	(R)	174.71 178.71 187.74 187.74 187.74 188.11 187.79 189.71 189.71 189.71 189.71 189.72 18
SEALS FOR CR	Single brush	AVG PRESS STATION 5	(PSIA)	637.57 7743.170 7743.60 7743.60 7743.60 7745.98 6645.98 665.00 775.04 775.02 775.02 775.02 775.03 77
: BRUSH	NO. 2	EN S AVG PRESS STATION 1	(PSIA)	761.07 764.07 764.07 764.07 764.07 764.07 764.07 764.07 764.07 764.07 766.06 766.26 766.26
RESEARCH PROGRAM	CONFIGURATION	FLUID: NITROGE RDG AVG SCANS		179 ALL SCNS 180 ALL SCNS 181 ALL SCNS 182 ALL SCNS 184 ALL SCNS 185 ALL SCNS 186 ALL SCNS 186 ALL SCNS 187 ALL SCNS 189 ALL SCNS 190 ALL SCNS 191 ALL SCNS 192 ALL SCNS 203 ALL SCNS 204 ALL SCNS 205 ALL SCNS 205 ALL SCNS 206 ALL SCNS 207 ALL SCNS 208 A

FLUID: NITROGEN

AVERAG LEAKAG RATE (LBM/S	00000000000000000000000000000000000000		600000000000
AVERAGE SHAFT SPEED (RPM)	25079:112:22 254998:112:22 254998:112:22 254998:113:22 254	\$	င်္ကေတြက်တဲ့ လိုက်တဲ့ လိုက်တဲ လိုက်တဲ့ လိုက်တဲ့ လိ လိုက်တဲ့ လိုက်တဲ့ လိ
AVG TEMP STATION 5 (R)	159-511 155-869 166.263 165.284 210.284 210.284 155.088 155.088 155.745 155.745 157.748 183.788 183.788 183.788 183.763 177.773 177.773 177.773 180.391 180.391	160.267 158.509 156.330 156.330 156.330 156.340 156.340 157.002 157.002 169.894 169.894 198.231 197.593 237.246	157.534 160.292 157.521 156.283 155.721 156.721 160.145 166.449 183.139
AVG TEMP STATION 4 (R)	152.86 153.87 165.33.08 150.05 150.05 150.05 150.05 150.05 150.05 150.05 163.28 163.28 163.28 163.28 163.28 163.28 163.28 163.28 163.28 163.28 163.28 163.28 163.28 163.28 163.28 163.28 163.28	151.13 151.13 151.13 151.13 151.13 150.06 150.06 179.22 179.22 179.22 179.22 179.22 179.22 179.22 179.22 179.22 179.22 179.22	154.57 154.57 152.75 151.63 151.72 152.86 153.92 156.57 161.97
AVG TEMP STATION 3 (R)	1553. 1553. 1553. 1553. 1553. 1553. 1550.	152.59 151.51 151.75 151.75 151.64 151.65 152.05 178.99 178.99 176.53 176.53 176.53 176.53	156.05 157.73 152.73 152.73 152.76 154.21 156.86 169.73
AVG TEMP STATION 1 (R)	150.056 150.056 150.057 150.05	150.051 150.051 150.051 150.051 160.05	1,5,92 152.76 152.76 151.78 151.80 153.18 154.17 156.74 166.27
AVG PRESS STATION 5 (PSIA)	587. 82 636.78 636.78 636.78 63.26 785.92 785.92 735.79 638.33 633.32 683.33 789.84 789.84 789.84 789.86 686.57 686.57 686.60 685.60	787.73 639.74 639.75 639.75 639.75 639.78 785.78 785.78 785.78 785.77 680.10 680.10 680.10 680.10	509.24 777.17 720.89 670.11 670.11 670.11 563.10 563.10 710.39 758.72 784.70
AVG PRESS STATION 4 (PSIA)	800.29 780.15 765.17 753.49 738.44 719.62 740.29 767.41 784.79 812.38 810.09	799.66 780.98 757.56 743.26 748.21 772.34 772.34 772.34 800.15	790.53 767.92 758.01 744.95 733.55 728.01 736.72 744.47 756.10 773.21
AVG PRESS STATION 3 (PSIA)	800.56 765.52 755.52 754.74 725.18 725.05 725.18 740.78 757.84 812.68 810.44	799.85 766.06 757.89 757.89 738.52 738.61 778.64 800.14 810.97	790.69 768.02 758.22 733.97 731.39 736.96 756.40 773.36
AVG PRESS STATION 1 (PSIA)	810.53 810.65 810.65 810.65 811.19 801.11 809.97 809.97 806.47 806.47 812.34 812.34 812.34 812.34 812.34 812.34 812.34 812.34 813.89	8809.90 8809.90 8809.90 8809.82 8810.33 8811.02 8801.38 8801.38 8801.38 8801.38 8801.39 8801.34 8801.34	807.72 800.54 797.14 792.22 788.84 788.84 783.03 782.41 782.73 783.60
ID: NITROGEN AVG SCANS P	293 ALL SCNS 2295 ALL SCNS 2295 ALL SCNS 2295 ALL SCNS 2297 ALL SCNS 3302 ALL SCNS 3303 ALL SCNS 3303 ALL SCNS 3313 ALL SCNS 3314 ALL SCNS 3315 ALL SCNS 3316 ALL SCNS 3317 ALL SCNS 3316 ALL SCNS 3317 ALL SCNS 3318 ALL SCNS 3318 ALL SCNS 3318 ALL SCNS 3316 ALL SCNS 331		ALLLLLLLLLLLLLLLLLLLLLLLLLLLLLLLLLLLLL
FLUID RDG		<i>โ</i> ล้ ค็ ค็ ค็ ค็ ค็ ค็ คิ	 କ୍ଷ୍ୟୁଲ୍ଲ ଅନ୍ୟୁକ୍ତ ଅନ୍

CONFIGURATION NO. 4 2 Brushes tightly packed .. positions 3 & 4

FLUID: NITROGEN RDG AVG SCANS		362 ALL SCNS 363 ALL SCNS 364 ALL SCNS 365 ALL SCNS 366 ALL SCNS 367 ALL SCNS 377 ALL SCNS 377 ALL SCNS 377 ALL SCNS 378 A	
N AVG PRESS STATION 1	(PSIA)	810. 21 810. 21 801. 32 805. 32 798. 43 791. 92 788. 67 787. 68 789. 787. 68 789. 787. 68 789. 787. 68 789. 787. 68 789. 787. 68 789. 789. 789. 789. 789. 789. 789. 789.	
AVG PRESS STATION 2	(PSIA)	810.49 805.57 805.57 805.57 805.57 807.53 792.33 792.33 792.33 792.33 793.10 804.81 807.85 794.55 794.55 794.55 795.68 807.83 807.83 807.83 808.81 799.87	
AVG PRESS STATION 5	(PSIA)	7.754.06.44 7.85.46.44 7.86.44 7.87.1.26 6.70.17 7.88.93 6.89.58 6.89.58 6.89.59 7.89.66 6.89.69 7.89.66 6.89.69 6.73.58	
AVG TEMP STATION 1	(R)	150.99 150.09 149.88 149.49 149.49 149.49 149.33 149.49 149.33 149.48 149.33 149.48 149.33 149.70	
AVG TEMP STATION 2	(R)	152.31 151.42 151.42 150.36 15	
AVG TEMP STATION 5	(R)	165.98 164.97 163.81 164.82 164.83 16	
AVERAGE SHAFT SPEED	(RPM)	50277.5.5.5.5.5.5.5.5.2.8.4.6.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2	
AVERAGE LEAKAGE RATE	(LBM/S)	0.127 0.127 0.127 0.236 0.236 0.236 0.345 0.369 0.369 0.369 0.369 0.265 0.265 0.265 0.252	
DELTA-P STA 1-5	(PSID)	23.77 51.06 74.65 1175.25 125.25 126.25 127.33 129.93 121.32 121.32 121.32 121.32 121.32 121.33 121.33 121.33 121.33 121.33 121.33 122.34 123.93	
DELTA-P STA 1-2	(PSID)	7.220 7.	

	DELTA-P STA 1-2	(PSID)	5-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0
	DELTA-P STA 1-5	(DISA)	22. 22. 22. 22. 22. 22. 22. 22. 22. 22.
	AVERAGE LEAKAGE	(LBM/S)	0.0053 0.
	AVERAGE SHAFT	(RPM)	22222222222222222222222222222222222222
	AVG TEMP STATION 5	(R)	100.053.32 100.053.32
	AVG TEMP STATION 2	(R)	150.150 150.178 150.17
•	AVG TEMP STATION 1	(R)	150.94 150.94 150.99 150.99 150.99 150.99 150.99 150.99 150.99 150.99 150.99 150.99 150.99 150.99 150.99 150.99 150.99 150.99
	AVG PRESS STATION 5	(PSIA)	7.86 616.23 616.23 616.23 616.23 606.23 606.23 606.33 606.
	AVG PRESS STATION 2	(PSIA)	8004-28 8004-28 8004-28 800-29 800-29 8004-28 8004-29
ı	AVG PRESS STATION 1	(PSIA)	793. 35 795. 55 795. 5
	AVG SCANS F		AALL SCNS AALL S
	FLUID:		44444444444444444444444444444444444444

CONFIGURATION NO. 5 3 Brushes equally space: pos 1,3,5

SEALS FOR

BRUSH

RESEARCH PROGRAM:

AVERAGE LEAKAGE RATE (LBM/S) AVERAGE SHAFT SPEED (RPM) 5 AVG TEMP STATION 5 175.839 167.559 167.559 167.559 167.559 167.559 167.559 167.559 163.277 163.285 163.286 163.286 163.287 163.289 4 AVG TEMP STATION 4 166.23 155.23 15 2 N AVG TEMP STATION 2 160.82 151.37 150.34 150.23 150.23 150.17 15 \blacksquare AVG TEMP STATION 1 1500.35 1500.3 AVG PRESS STATION 5 796.60 771.03 701.30 701.30 701.30 701.30 701.30 701.30 701.30 701.30 701.57 701.30 701.57 701.57 701.57 701.57 701.57 701.57 AVG PRESS STATION 4 797.54 775.04 775.04 738.36 713.35 713.35 692.90 677.12 677.12 677.12 671.51 671.51 709.46 712.61 745.13 768.45 779.67 766.69 778.30 720.36 720.36 720.36 720.36 730.37 740.50 724.77 746.58 768.58 (PSIA) AVG PRESS STATION 2 779.55 773.09 773.09 768.18 744.01 729.87 727.39 727.39 727.39 727.39 727.39 727.39 (PSIA) 776.70 776.70 776.70 776.70 771.70 772.98 772.98 772.98 772.108 772.108 772.108 772.135 773.30 774.20 775.66 779.80 SS 797.62 778.76 7778.76 AVG PRES STATION (PSIA) D: NITROGEN AVG SCANS A FLUID: RDG A

		AVERAGE LEAKAGE RATF	(LBM/S)	0.14 0.00 0.00 0.00 0.00 0.12 0.17 0.13 0.01 0.00 0.00 0.00 0.00 0.00 0.00	0.000000000000000000000000000000000000		0.00 0.00 0.19 0.20 0.20 0.17 0.17	0.000000000000000000000000000000000000
200 1318		AVERAGE SHAFT SPFFD	(RPM)	1499899 1499899 1499899 1499899 1499899 1499899 1499899 1499899 1499899 149989 149989 149989 149989 149989 149989 149989 149989 149989 149989 149989 14998 1	25240.3 25240.3 25240.3 252138.8 25247.5 25182.5 25182.5 25174.1 25337.2	ၛၮၮၮၮၮၮၮၮၮၮၮ ၯၜၴၜၟၜၟၜၜၜၜၜၜၜၜၜၜ ႜ	35117.5 35117.5 35117.3 35021.3 35245.3 35245.3 3711.3 32790.0 34045.9 34214.4	
UNC 1 EK : 14.		AVG TEMP STATION 5	(R)	159.955 161.353 1864.935 1874.607 157.879 155.127 155.127 156.731 156.731 158.415 159.901 168.278	185.7/5 206.729.431 195.048 185.243 187.051 181.362 181.362 185.399	177.785 163.045 169.045 159.067 159.321 159.360 159.296 159.298 160.213	174.346 235.007 234.636 203.608 207.198 192.043 191.619 196.647 203.356	168.861 161.930 161.930 160.733 160.733 160.115 160.301 160.633 162.284 173.049
רבורכ פאצ		AVG TEMP STATION 4	(R)	154.68 155.27 158.08 173.56 173.56 151.17 151.21 153.50 157.32 165.22 166.08	185.02 176.14 176.14 163.64 162.20 162.52 164.34 164.34	166.22 166.22 148.19 148.83 148.83 148.73 148.65 168.65 168.65	268.12 197.18 174.15 177.01 163.00 165.90 171.34 171.34	153.13 153.13 153.13 150.78 150.31 150.34 150.39 151.51 162.81
וו: רור		AVG TEMP STATION 2	(R)	153.49 155.24 155.24 155.24 150.93 150.99 154.96 154.96 158.33 161.64	11.5.2.2 163.3.30 163.3.30 159.0.1 159.0.34 159.93 159.93 159.93	168.53 168.53 168.53 168.53 168.53 168.53 169.51	153.78 212.16 212.16 167.26 166.25 161.52 165.30 165.30 165.30	151.35 151.35 150.60 150.14 149.89 149.71 149.84 149.93 150.01 150.70
IESI FALILIIT		AVG TEMP STATION 1	(R)	150.84 150.78 150.78 150.39 150.34 150.15 150.14 155.40 155.40 155.40 166.00	153.47 1552.84 1552.07 151.09 152.36 152.36 152.36	148.15 147.81 147.82 147.83 147.99 148.03 148.03 147.87 147.87	147.85 158.26 157.48 157.53 157.53 156.14 156.96 157.62	150.08 150.10 150.10 149.97 149.88 149.88 149.95 150.07 150.06 150.84
£	e: pos 1,3,5	AVG PRESS STATION 5	(PSIA)	603.47 657.34 7758.50 7758.71 7750.31 7720.69 650.17 650.17 550.83 754.64 704.60	783.49 7057.91 659.57 559.11 557.11 669.46 669.40 768.56	752.23 754.17 754.17 703.11 703.11 705.23 706.68 706.68	781.77 760.49 760.49 661.36 661.36 601.64 593.57 593.85 644.49	747.27 680.42 628.73 577.79 522.77 571.62 618.69 668.68
RYOGENIC APP	lually space:	AVG PRESS STATION 4	(PSIA)	780.29 766.91 741.04 715.79 694.12 691.15 674.54 691.91 703.29 716.82 741.73	783.67	782.98 768.58 741.57 714.98 683.10 663.10 665.67 743.43 768.85	782.73	749.40 714.66 683.11 655.67 600.92 625.65 625.65 674.02 771.26 771.26
ALS FOR C	8 Brushes eq	AVG PRESS STATION 2	(PSIA)	779.87 773.26 759.50 746.14 738.00 722.21 749.42 761.46	~	781.97 775.39 763.33 751.36 741.30 726.98 737.55 747.09 757.16	81.	756.66 740.01 726.49 713.44 700.00 686.37 695.85 705.54 714.93 725.89 739.96
RAM: B	NO. 5	AVG PRESS STATION 1	(PSIA)	778.58 778.69 778.99 778.91 778.91 778.28 778.35 776.25 777.94 773.14 775.45				
	FIGURATION	FLUID: NITROGEN RDG AVG SCANS		529 ALL SCNS 530 ALL SCNS 531 ALL SCNS 532 ALL SCNS 534 ALL SCNS 536 ALL SCNS 536 ALL SCNS 539 ALL SCNS 539 ALL SCNS 540 ALL SCNS 541 ALL SCNS	######################################	44444444444		

AVERAGE	LEAKAGE RATE (LBM/S)	0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.
AVERAGE	SPEED (RPM)	22222222222222222222222222222222222222
AVG TEMP	(R)	155. 368 155. 368 155. 368 155. 329 155. 329 155. 329 155. 329 155. 329 155. 329 155. 325 165. 325 165
AVG TEMP	(R)	1550.054 1650.054 1650.055 1650.0
AVG TEMP	S!A! 10N 3 (R)	155.39 155.39 155.30 15
AVG TEMP	= ~	115050992222238888888888888888888888888888888
AVG PRESS	8 0.	757.757.757.757.757.757.757.757.757.757
AVG PRESS	<u>z</u> _	744.8 777.7 778.8 778.8 778.8 778.8 778.8 778.8 778.8 778.8 777.8 778.8
AVG PRESS	110N S1A)	775.73.27.75.75.75.75.75.75.75.75.75.75.75.75.75
AVG PRESS	<u> </u>	781.39 781.28 781.28 781.28 780.70 780.70 780.70 780.70 780.70 781.57 781.57 781.57 784.15 784.15 784.15 787.10 787.10 787.10 787.10 787.10 787.10 787.10 787.10 787.10
FLUID: NITROGEN RDG AVG SCANS		594 ALL SCNS 595 ALL SCNS 595 ALL SCNS 597 ALL SCNS 597 ALL SCNS 599 A

AVERAGE AVG TEMP AVG TEMP AVG TEMP FLUID: NITROGEN
RDG AVG SCANS AVG PRESS AVG PRESS AVG PRESS AVG TEMP

VERAGE EAKAGE SATE	(L BM /S)	00.00000000000000000000000000000000000	
AVERAGE / SHAFT SPEED	(RPM)	335043.4 149228.1 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 14923.7 16033.7 1772.7 16033.7 16	
AVG TEMP STATION 5	(R)	158. 111 155. 470 155. 470 155. 470 155. 470 155. 470 155. 470 155. 470 155. 470 155. 470 155. 488 155. 688 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 588 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 155. 388 160. 370 173. 388	
AVG TEMP STATION 4	(R)	151.82 1550.83	
AVG TEMP STATION 2	(R)	1499 1550.53 1499.99 1499.99 1499.99 1499.99 1500.99 177.65 177.6	
AVG TEMP STATION 1	(R)	149.50.59 150.059 150.	
AVG PRESS STATION 5	(PSIA)	763.41 763.41 763.84 5613.94 6613.94 6613.94 765.72 765	
AVG PRESS STATION 4	(PSIA)	771. 7744.90 7744.90 7724.90 7727.25 7727.25 7727.25 7727.25 7727.25 7727.25 7737.90 7737.90 7737.73	
AVG PRESS STATION 2	(PSIA)	775-75-75-75-75-75-75-75-75-75-75-75-75-	
WG PRESS	(PSIA)	780.44 7779.95 7779.95 7779.95 7779.95 7779.95 7779.95 7782.95 7779.95	
FLUID: NITROGEN RDG AVG SCANS A		662 ALL SCNS 665 ALL SCNS 666 ALL SCNS 666 ALL SCNS 667 ALL SCNS 667 ALL SCNS 677 ALL SCNS 677 ALL SCNS 677 ALL SCNS 678 ALL SCNS 678 ALL SCNS 678 ALL SCNS 679 ALL SCNS 670 ALL SCNS 670 ALL SCNS 670 ALL SCNS 670 ALL SCNS 671 ALL SCNS 672 ALL SCNS 673 ALL SCNS 673 ALL SCNS 674 ALL SCNS 675 ALL SCNS 675 ALL SCNS 675 ALL SCNS 675 ALL SCNS 676 ALL SCNS 677 ALL SCNS 678 ALL SCNS 678 ALL SCNS 678 ALL SCNS 678 ALL SCNS 679 ALL SCNS 670 A	

BAROMETER: 14.165 PSIA BRUSH SEALS FOR CRYOGENIC APPLICATIONS TEST FACILITY: CCL - CELL2 Single Brush - position 1 œ RESEARCH PROGRAM: CONFIGURATION NO.

DELTA-P STA 1-5 (PSID)	25.25.25.25.25.25.25.25.25.25.25.25.25.2
AVERAGE LEAKAGE RATE (LBM/S)	0.000000000000000000000000000000000000
AVERAGE SHAFT SPEED (RPM)	ݵݡݥݡݡݡݡݡݡݡݡݡݡݡݡݥݡݥݡݥݡݥݡݥݡݥݡݥݡݥݡݥݡݥݡݥݡݥݥݥݡݥݥݥݡݥݡ
AVG TEMP STATION 5 (R)	155. 25 4 4 4 4 8 8 8 8 4 4 8 4 8 4 8 8 8 4 2 5 2 5 2 5 2 5 2 5 2 5 2 5 2 5 2 5 2
AVG TEMP STATION 1 (R)	150.151 150.083 160.083 160.08
AVG PRESS STATION 5 (PSIA)	7.3.7.4.6. 7.3.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.
OGEN AVG PRESS STATION 1 (PSIA)	789.187 785.133 785.333 785.40 785.40 785.93
FLUID: NITROGEN RDG SCAN	740 740 740 740 740 740 740 740

	DELTA-P STA 1-5	(PSID)	251.53 246.81 254.64 254.64 277.61 277.61 277.61 277.61 277.61 277.61 277.61 277.61 277.61 288.93 277.76 288.93 305.24 30
	AVERAGE LEAKAGE DATE	(S/WBJ)	0.3952 0.3872 0.3872 0.3872 0.3872 0.3872 0.3872 0.3872 0.3972 0.3973 0.
	AVERAGE SHAFT Speen	(RPM)	ဎႋၹၟၹၟႜၹၟၹၟၹၟၹၟၹၟၹၟၹၟၹၟၹၟၹၟၹၟၹၟၹၟၹၟၹၟၹၟၹၟ
	AVG TEMP STATION 5	(R)	153.17 15
- position l	AVG TEMP STATION 1	(R)	149.489 149.489 149.659 149.977 149.977 149.977 149.659
Single Brush	AVG PRESS STATION 5	(PSIA)	514.77 520.68 520.68 5497.59 5607.68 5607.68 5607.68 5607.69 5607.6
NO. 8	EN AVG PRESS STATION 1	(PSIA)	766. 30 767. 30 767. 30 767. 30 765. 3
CONFIGURATION	FLUID: NITROGEN RDG SCAN		740 55 740 55 740 55 740 55 740 55 740 65 740 65 740 65 740 65 740 65 740 65 740 65 740 65 740 65 740 72 740 88 740 88 740 88 740 99 740 99 740 99 740 99 740 99 740 99 740 99 740 99 740 100 740 100

RESEARCH PROGRAM: BRUSH SEALS FOR CRYOGENIC APPLICATIONS TEST FACILITY: CCL - CELL2 BAROMETER: 14.165 PSIA

RESEARCH PROGRAM	RAM: BRUSH No. 8	SEALS FOR CRY Single Brush	CRYOGENIC APPL. sh - position]	APPLICATIONS TES	FACILITY:	ננו - נפווצ	BARUME EKT. 1
FLUID: NITROGEN RDG SCAN A S	AVG PRESS STATION 1 (PSIA)	AVG PRESS STATION 5 (PSIA)	AVG TEMP STATION 1 (R)	AVG TEMP STATION 5 (R)	AVERAGE SHAFT SPEED (RPM)	AVERAGE LEAKAGE RATE (LBM/S)	DELTA-P STA 1-5 (PSID)
	755.15	335.07	149.77	153.80	-6.3	0.407	420.08
	755.15 755.15	337.30 341.95	149.77 149.89	153.64 153.80	6.0.	0.430 0.418	417.85
	754.90 755.01	334.80 343.13	149.77 149.54	153.80 153.80	. 4.	0.415	420.10 411.89
	755.07	342.85 354.10	149.53 149.83	153.80 153.80	و. 4.0	0.415	412.22 401.44
	754.03	315.70	149.42	153.80	94	0.431	438.32
	752.60	297.71	149.65	153.95	90,4	0.426	454.88
	752.50	295.43	149.71	153.80	999	0.430	457.07
	753.22	300.15	149.71	153.96	4.	0.425	453.07
	753.08 752.83	305.57 306.67	149.54 149.89	153.80 153.72	2. d.	0.42/	446.16
	752.15	2 83.4 8 2 80. 15	149.65 149.65	153.64 154.27	-6- -6.3	0.432 0.441	468.67 472.10
. — –	751.49	270.92	149.54	154.11	6.3	0.431	480.57 478.69
	751.02	265.84	149.54	153.96		0.433	485.18
	750.89	265.64	149.71	153.49	, 6, 4	0.429	485.26 478 06
	750.58	262.58	149.77	153.80	. 6. 6.	0.456	487.99
	749.56 749.24	248.70 242.31	149.65	154.27	4.4.	0.448	500.85 506.93
	749.14 749.70	241.55 239.94	149.83 149.89	154.03 154.03	-6.3 4.6.3	0.441	509.76 509.76
	749.32	240.85	149.65	154.27 153.41	4.6-3	0.444 0.440	508.47 506.53
••••	750.18	250.02	149.65	153.80	,	0.440	500.17
• • • •	749.52	253.00	149.95	153.33	, m	0.452	496.52 503 98
	749.52	242.37	149.65	153.65	9.00	0.447	507.15
	749.17	238.42 237.03	149.83	153.41	4.0	0.445	511.62
	749.11 749.21	237.73 241.33	149.59 149.65	153.80		0.443	511.38
	748.72	247.25 255.36	149.89	153.72	2.00 4.00	0.436	501.48 495.02
	750.05 748.93	254.11 243.77	149.65 149.65	153.57	ကို ကို	0.44/	495.94 505.15
	748.96 749.21	242.65 239.32	149.48 149.65	153.64 154.11	-6-4 -6-4	0.442	506.31 509.89
	748.76 748.65 748.65	236.12 237.30 238.35	149.60 149.71 149.59	153.5/ 153.80 153.57	5 4 4 5 4 4	0.442 0.441 0.441	511.34 510.23
	748.41	245.85 251.40	149.71	153.65 153.80	44	0.437	502.56 497.44
740 161 740 162 740 163	749.21 748.89 740.17	255.02 247.94 243.77	149.83 149.83 140.95	153.65 153.88 153.96	2.00 A	0.446 0.442 0.443	494.18 500.95 505.41
	748.37	239.61	149.83	152.87	4.6-	0.442	508.76

BAROMETER:		DELTA-P STA 1-5 (PSID)	512. 69 511. 47 509. 49 509. 49 509. 69 509. 69 509. 69 509. 69 509. 69 509. 69 509. 69 509. 69 509. 76 509. 76 509
ככר - כברדק		AVERAGE LEAKAGE RATE (LBM/S)	0.000000000000000000000000000000000000
ST FACILITY:		AVERAGE SHAFT SPEED (RPM)	ĠĠġĠĠġġġĠĠġĠġġĠġġġġġġġġġġġġġġġġġġġġġġġ
ICATIONS TEST		AVG TEMP STATION 5 (R)	153.88 154.35 154.35 154.35 154.35 154.27 154.27 154.27 154.27 154.50 154.42 154.42 154.42 154.42 154.43 154.52 154.35
CRYDGENIC APPLICATIONS	- position	AVG TEMP STATION 1 (R)	149.73 149.83 149.83 149.83 149.83 149.83 149.65 149.83 149.83 149.83 149.83 150.07 150.07 150.07 150.01 150.03 150.03 150.03 150.03 150.03 150.03
SEALS FOR CR	Single Brush	AVG PRESS STATION 5 (PSIA)	236.556 238.556 238.556 238.556 238.556 2238.01 2238.01 2238.01 2236.02 2236.71 2236.72 2236.72 2236.72 2236.72 2236.72 2236.72 2236.72 2236.73 2236.73 2236.73 2236.73 2236.73 2236.73 2236.74 2236.73 2366.73 2366.7
: BRUSH	NO. 8	EN AVG PRESS STATION 1 (PSIA)	748.75 748.75 748.75 748.75 748.75 748.55 748.55 748.55 748.55 748.66 748.66 748.66 748.66 748.66 748.76
RESEARCH PROGRAM	CONFIGURATION	FLUID: NITROGEN RDG SCAN	740 165 740 166 740 166 740 169 740 170 740 170 740 171 740 173 740 183 740 183 740 202 740 203 740 203 740 203 740 203 740 203 740 213 740 213 740 213 740 213 740 213 740 213 740 213

14.165 PSIA

SS SS	CONFIGURATION NO	ON NO. 8	Single Brush	- position	-				
(PSIA) (PSIA) (R) (R) (R) (R) (R) (R) (R) (R) (R) (R	NITR	OGEN AVG PRESS STATION 1	AVG PRES STATION	AVG TEMP STATION 1	AVG TEMP STATION 5	AVERAGE SHAFT	AVERAGE LEAKAGE	DELTA-P STA 1-5	
742.64 138.23 150.36 1155.36 -6.3 0.455 742.56 1138.23 150.36 1156.38 1156.28 1150.29 1150.29 1154.89 1157.78 1150.59 1150.29 1150.29 1154.89 1157.78 1150.59 1150.29 1150.29 1154.89 1157.78 1150.59 1150.29		(PSIA)	(PSIA)	(R)	(R)	(RPM)	(LBM/S)	(PSID)	
772.56 138.86 150.48 154.89 154.89 154.89 154.89 154.89 154.89 156.24 154.89 156.24 154.89 156.24 154.89 156.27 156.28 15	20	742.64	138.23	150.36	155.36	-6.3	0.454	604.41	
742.53 143.78 150.24 155.82 -9.4 0.048 742.53 143.78 150.24 155.82 -9.4 0.048 742.53 140.80 150.18 150.42 155.82 -9.4 0.048 742.82 140.80 150.18 150.18 154.81 -9.4 0.0455 742.83 119.21 150.18 150.18 154.89 -9.4 0.0455 741.83 119.21 150.18 150.18 154.89 -6.3 0.0455 741.85 119.21 150.18 150.18 154.89 -6.3 0.0455 741.85 119.21 150.18 150.18 154.89 -6.3 0.0455 741.85 119.81 150.18 150.18 154.89 -6.3 0.0455 741.85 119.81 150.18 150.18 154.89 -6.3 0.0455 740.89 100.89 1100.18 154.89 -6.3 0.0455 740.89 100.89 1100.18 154.89 -6.3 0.0455 740.89 100.89 1100.18 154.89 -6.3 0.0455 740.89 100.89 1100.18 154.43 -6.3 0.0455 740.89 1100.19 150.18 154.43 -6.3 0.0455 740.89 1100.19 150.18 154.43 -6.3 0.0455 740.89 1100.19 150.18 154.43 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19 154.45 -6.3 0.0455 740.89 1100.19	25	742.56	138.86	150.48	154.89	4.0	0.455	603.70	
747.78 747.78 747.78 747.89 74	233	742.53	143.78	150.24	154.82	4.0	0.448	598-75	
742.25 143.86 150.13 154.50 -5.3 0.455 742.26 143.86 150.13 154.50 -5.3 143.86 150.13 154.50 -5.3 143.86 150.13 154.50 -5.3 143.86 150.13 154.50 -5.3 143.86 150.13 154.50 -5.3 143.86 150.13 154.50 -5.3 142.50 145	52	742.78	150.86	150.42	154-81	-6.3	0.455	591.92	
742.26 741.28 742.26 741.28 741.28 741.28 741.28 741.28 741.28 741.28 741.28 741.28 741.28 741.28 741.28 741.28 741.28 741.28 741.28 741.29 741.20	256	742.95	143.86	150.13	154.50	4.6	0.455	599.09	
741.83 126.08 150.18 154.81 -6.3 0.454 741.35 120.04 150.30 150.30 154.81 -6.3 0.455 741.35 120.04 150.30 150.30 154.50 -6.3 0.455 741.59 120.04 150.30 150.30 154.51 -6.3 0.455 741.59 118.03 150.30 154.43 -6.3 0.455 740.89 100.59 150.24 150.30 154.43 -6.3 0.455 740.73 118.03 150.30 150.24 154.35 -6.3 0.455 740.22 100.10 11 150.13 150.13 150.13 154.43 -6.3 0.455 740.22 100.10 11 150.13 150.13 154.42 -6.3 0.455 740.22 100.10 11 150.13 150.13 154.42 -6.3 0.455 740.22 100.10 11 150.13 150.13 154.42 -6.3 0.455 740.22 100.10 11 150.13 150.13 154.42 -6.3 0.455 740.25 87.89 150.10 154.43 -9.4 0.455 740.26 100.87 150.10 154.43 -9.4 0.455 740.27 150.29 150.20 150.20 154.43 -9.4 0.455 740.28 150.29 150.20 150.20 154.43 -9.4 0.455 740.28 150.29 150.20 150.20 154.43 -9.4 0.455 740.28 150.29 150.20 150.20 154.43 -9.4 0.455 740.28 150.29 150.20 150.20 154.43 -9.4 0.455 740.28 150.29 150.20 150.20 154.43 -9.4 0.455 740.28 150.29 150.20 150.20 154.43 -9.4 0.455 740.28 150.29 150.20 150.20 154.43 -9.4 0.455 740.28 150.29 150.20 150.20 154.43 -9.4 0.455 740.20 150.20 150.20 150.20 154.43 -9.4 0.455 740.20 150.20 150.20 150.20 154.43 -9.4 0.455 740.20 150.20 150.20 150.20 154.43 -9.4 0.455 740.20 150.20 150.20 150.20 154.43 -9.4 0.455 740.20 150.20 150.20 150.20 154.43 -9.4 0.455 740.20 150.20 150.20 150.20 154.43 -9.4 0.455 740.20 150.20 150.20 150.20 154.43 -9.4 0.455 740.20 150.20 1	28	742.26	137.33	150.13	154.50	 •	0.455	604.93	
741.35 741.35 741.35 741.35 741.35 741.35 741.52 741.52 741.52 741.52 741.53 741.54 741.55 741.56 741.57 741.59 741.59 740.70 740.70 74	23	741.83	126.08	150.18	154.81	-6.3	0.454	615.75	
741.28 124.74 150.30 154.10 -6.3 0.455 741.28 124.74 150.30 154.11 -6.3 0.455 741.03 113.79 100.20 150.20 150.30 154.11 -6.3 0.455 740.29 100.29 150.20 150.20 150.20 154.35 -6.3 0.455 740.29 100.20 150.20 150.20 150.20 150.30 154.13 -6.3 0.455 740.29 100.20 150	83	741.35	119.21	150.30	154.97	6 .3	0.455	622.14	
742.16 126.43 150.07 153.10 -6.3 0.455 741.05 118.03 118.03 150.36 154.51 0.454 740.05 118.03 118.03 150.36 154.51 0.454 740.02 118.03 118.03 150.36 150.24 154.35 -9.4 0.454 740.02 118.03 150.24 154.35 -9.4 0.455 740.02 100.59 150.18 150.18 154.19 -6.3 0.455 740.02 100.59 150.18 150.18 154.19 -6.3 0.455 740.02 100.59 150.18 150.18 154.42 -6.3 0.455 740.02 100.59 150.18 150.18 154.42 -6.3 0.455 740.02 100.03 150.18 150.18 154.42 -6.3 0.455 740.02 100.03 150.18 150.18 154.42 -6.3 0.455 740.02 100.03 150.19 154.42 -6.3 0.455 740.02 100.03 150.19 150.10 154.42 -6.3 0.455 740.02 100.03 150.10 150.19 154.42 -9.4 0.455 740.02 100.03 150.03 150.10 154.43 -9.4 0.455 740.02 100.03 150.03 150.03 154.43 -9.4 0.455 740.02 100.03 150.03 154.43 -9.4 0.455 740.02 100.03 150.03 154.43 -9.4 0.455 740.02 100.03 150.03 154.43 -9.4 0.455 740.03 150.03 150.03 154.43 -9.4 0.455 740.03 150.03 150.03 154.43 -9.4 0.455 740.03 150.03 150.03 154.43 -9.4 0.455 740.03 150.03 150.03 154.43 -9.4 0.455 740.03 150.03 150.03 154.43 -9.4 0.455 740.03 150.03 150.03 154.43 -9.4 0.455 740.03 150.03 150.03 154.43 -6.3 0.455 740.03 150.03 150.03 154.43 -9.4 0.455 740.03 150.03 150.03 154.43 -6.3 0.455 740.03 150.03 150.03 154.43 -9.4 0.455 740.03 150.03 150.03 154.43 -6.3 0.455 740.03 150.03 150.03 154.43 -6.3 0.455 740.03 150.03 150.03 154.43 -6.3 0.455 740.03 150.03 150.03 154.43 -6.3 0.455 740.03 150.03	33.	741.58	120.04	150.35	154.13	7.0°	0.452	616.75	
741.59 118.03 150.36 154.45 -6.3 0.454 740.89 107.69 107.69 150.24 154.45 -6.3 0.454 740.89 107.69 107.69 150.24 154.45 -6.3 0.455 740.73 98.93 150.18 150.18 154.19 -6.3 0.455 740.73 98.93 150.18 150.18 154.42 -6.3 0.455 740.50 107.69 107.69 150.18 154.42 -6.3 0.455 740.50 107.69 107.69 150.18 154.42 -6.3 0.455 740.20 107.60 107.60 107.87 150.19 154.42 -6.3 0.455 740.20 107.60 107.87 150.19 154.42 -6.3 0.455 740.20 107.60 107.60 107.87 150.19 154.42 -6.3 0.455 740.20 107.60 107.80 150.10 154.42 -6.3 0.455 740.20 107.60 107.80 150.10 154.43 -9.4 0.455 740.20 107.60 107.60 107.80 150.10 154.43 -9.4 0.455 740.20 107.60 107.60 107.60 150.10 154.43 -9.4 0.455 740.20 107.60 107.	233	742.16	126.43	150.07	153.10	-6.3	0.455	615.73	
741.03 113.79 1150.24 154.35 -9.4 0.454 740.79 100.59 150.24 154.35 -6.3 0.4554 740.79 100.59 150.24 154.35 -6.3 0.4554 740.29 100.59 130.18 154.19 -6.3 0.4554 740.20 100.59 130.18 154.19 -6.3 0.4555 740.20 105.32 150.18 154.42 -6.3 0.4555 740.20 105.32 150.18 154.42 -6.3 0.4555 740.20 105.32 150.18 154.42 -6.3 0.4555 740.20 105.32 150.18 154.43 -9.4 0.4555 740.20 105.32 150.19 154.42 -9.4 0.4555 740.20 105.32 150.19 154.42 -9.4 0.4555 740.20 105.30 154.42 -9.4 0.4555 740.20 105.30 154.42 -9.4 0.4555 740.20 150.10 154.42 -9.4 0.4555 740.20 150.10 154.43 -9.4 0.4555 740.20 150.10 154.43 -9.4 0.4555 740.20 150.10 154.43 -9.4 0.4555 740.20 150.10 154.43 -9.4 0.4555 740.20 150.10 154.43 -9.4 0.4555 740.20 150.10 154.43 -9.4 0.4555 740.20 150.10 154.43 -9.4 0.4555 740.20 150.10 154.43 -9.4 0.4555 740.20 150.10 150.10 154.43 -9.4 0.4555 740.20 150.10 150.10 154.43 -9.4 0.4555 740.20 150.10 150.10 154.43 -9.4 0.4555 740.20 150.10 150.10 154.43 -9.4 0.4555 740.20 150.10 150.10 154.20 -9.4 0.4555 740.20 150.10 150.20 154.43 -9.4 0.4555 740.20 150.10 150.20 154.43 -9.4 0.4555 740.20 150.20 150.20 154.43 -9.4 0.4555 740.20 150.20 150.20 154.43 -9.4 0.4555 740.20 150.20 150.20 154.43 -9.4 0.4555 740.20 150.20 150.20 154.43 -9.4 0.4555 740.20 150.20 150.20 154.43 -9.4 0.4555 740.20 150.20 150.20 154.43 -9.4 0.4555 740.20 150.20 150.20 154.43 -9.4 0.4555 740.20 150.20 150.20 154.43 -9.4 0.4555 740.20 150.20	234	741.59	118.03	150.36	154.51		0.454	623.57	
740.789 100.799 150.24 154.66 -6.3 0.455 740.789 100.599 150.18 154.42 -6.3 0.455 740.789 100.789 150.18 150.18 154.42 -6.3 0.455 740.22 101.01 150.18 154.42 -6.3 0.455 740.22 101.01 150.18 154.42 -6.3 0.455 740.22 101.01 150.18 154.42 -6.3 0.455 740.22 101.01 150.18 154.42 -6.3 0.455 740.22 101.01 150.19 154.27 -6.3 0.455 740.22 101.01 150.19 154.27 -6.3 0.455 740.22 101.01 150.19 154.27 -6.3 0.455 740.22 101.01 150.19 154.42 -6.3 0.455 740.22 101.01 150.19 154.42 -6.3 0.455 740.22 101.01 150.19 154.42 -6.3 0.455 740.22 150.10 154.27 -9.4 0.455 740.25 150.10 154.27 -9.4 0.455 740.25 150.10 154.27 -9.4 0.455 740.25 74	235	741.03	113.79	150.30	154.43	ę. P	0.454	62.729	
740.29 99.13 150.19 154.35 -6.3 0.455 740.29 98.03 150.18 154.42 -6.3 0.455 740.20 100.83 150.18 154.42 -6.3 0.455 740.20 100.83 150.18 154.42 -6.3 0.455 740.20 100.83 150.18 154.42 -6.3 0.455 740.20 100.83 150.18 154.42 -6.3 0.455 740.20 100.83 150.19 154.27 -6.3 0.455 740.20 100.83 150.19 154.27 -6.3 0.455 740.20 87.09 150.19 154.43 -9.4 0.455 740.20 87.09 150.20 154.43 -9.4 0.455 740.20 87.09 150.30 154.42 -9.4 0.455 740.20 87.00 150.30 154.42 -9.4 0.455 740.20 87.00 150.30 154.43 -9.4 0.455 740.20 87.00 150.30 154.43 -9.4 0.455 740.20 87.00 150.30 154.43 -9.4 0.455 740.20 87.00 150.30 154.43 -9.4 0.455 740.20 87.00 150.30 154.43 -9.4 0.455 740.20 87.00 150.30 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 87.00 150.20 154.43 -9.4 0.455 740.20 150.20 154.20 154.20 -9.4 0.455 740.20 150.20 154.20 154.20 -9.4 0.455 740.20 150.20 150.20 154.20 -9.4 0.455 740.20 150.20 150.20 154.20 -9.4 0.455 740.20 150.20 154.20 -9.4 0.455 740.20 150.20 150.20 154.20 -9.4 0.455 740.20 150.20 150.20 154.20 -9.4 0.455 740.20 150.20 150.20 154.20 -9.4 0.455 740.20 150.20 150.20 154.20 -9.4 0.455 740.20 150.20 150.20 154.20 -9.4 0.455 740.20 150.20 150.20 154.20 -9.4 0.455 740.20 150.20 154.20 154.20 -9.4 0.455 740.20 150.20 154.20 154.20 -9.4 0.455 740.20 150.20 154.20 154.20 -9.4 0.455 740.20 150.20 154.20 154.20 -9.4 0.455 740.20 150.20 154.20 154.20 -9.4 0.20 150.20 154.20 150.20 154.20 1	737 737	740.89	100.59	150.24	154.66	1.09	0.454	640.19	
740,73 98.93 156,18 154,19 -6.3 0,455 740,36 98.93 156,18 154,42 -6.3 0,454 740,36 10.87 150,18 154,44 -6.3 0,455 740,06 100.87 150,18 154,43 -6.3 0,455 740,06 100.87 150,18 154,43 -6.3 0,455 740,06 100.87 150,19 154,43 -6.3 0,455 740,29 88.04 150,19 154,43 -6.3 0,455 739,29 88.04 150,10 154,43 -6.3 0,455 739,28 88.04 150,10 154,43 -6.3 0,455 739,56 88.05 150,00 154,43 -6.3 0,455 739,56 88.05 150,00 154,43 -6.3 0,455 739,10 154,27 -9.4 0,455 739,10 150,10 154,43 -6.3 0,455 739,10 150,10 154,43 -6.3 0,455 739,10 150,10 154,43 -6.3 0,455 739,10 150,10 154,43 -6.3 0,455 739,10 150,10 154,43 -6.3 0,455 739,10 150,10 154,43 -6.3 0,455 738,10 150,10 154,43 -6.3 0,455 738,10 150,10 154,43 -6.3 0,455 738,10 150,10 154,43 -6.3 0,455 738,10 150,10 154,13 -6.3 0,455 738,10 150,10 154,13 -6.3 0,455 738,10 150,10 154,13 -6.3 0,455 738,10 150,10 154,13 -6.3 0,455 738,10 150,10 150,10 154,13 -6.3 0,455 738,10 150,10 150,10 154,13 -6.3 0,455 738,14 168,14 150,17 154,17 -6.3 0,455 738,14 168,14 150,17 154,17 -6.3 0,455 738,14 168,14 150,17 154,13 -6.3 0,455 738,14 168,14 150,17 154,13 -6.3 0,455 738,14 168,14 150,17 154,13 -6.3 0,455 738,14 168,14 150,17 154,13 -6.3 0,455 738,14 168,14 150,17 154,13 -6.3 0,455 738,14 168,14 150,17 154,13 -6.3 0,455 738,14 168,14 150,17 154,13 -6.3 0,455 738,14 168,14 150,17 154,13 -6.3 0,455 738,14 150,1	238	740.29	99.13	150.19	154.35	6.3	0.455	641.16	
740.20 74	533	740.73	98.93	150.18	154.19	-6.3	0.455	641.80	
740.30 740.30 740.30 740.30 740.30 740.30 740.30 740.26 74	240	740.36	101.03	150.18	154.44	9.00	0.455	639.22	
740.06 100.87 150.19 154.27 -6.3 0.455 740.26 87.89 150.01 154.27 -6.3 0.455 740.26 87.89 150.01 154.82 -9.4 0.455 739.88 83.31 150.30 154.43 -9.4 0.455 739.88 83.72 150.30 154.43 -9.4 0.455 739.88 83.72 150.30 154.43 -9.4 0.455 739.56 82.69 150.30 154.43 -9.4 0.455 739.56 82.69 150.30 154.43 -9.4 0.455 739.57 83.03 150.30 154.43 -9.4 0.455 739.57 83.03 150.30 154.43 -9.4 0.455 739.51 738.73 69.01 150.19 154.51 -9.4 0.455 738.73 69.01 150.19 154.43 -9.4 0.455 738.73 69.01 150.19 154.43 -9.4 0.455 738.58 69.01 150.19 154.43 -9.4 0.455 738.58 69.01 150.07 154.58 -9.4 0.455 738.58 69.01 150.07 154.58 -9.4 0.455 738.58 69.01 150.07 154.58 -9.4 0.455 738.58 69.01 150.07 154.50 -6.3 738.58 69.69 149.57 154.58 -9.4 0.455 738.58 69.69 149.77 154.50 -6.3 738.58 69.63 149.77 154.11 -9.4 738.58 69.01 150.13 154.43 -9.4 9.4 738.58 68.50 150.13 154.43 -9.4 9.4 738.58 69.01 150.13 154.43 -9.4 9.4 738.58 69.01 150.13 154.43 -9.4 9.4 738.59 69.01 150.13 154.43 -9.4 9.4 738.59 69.01 150.13 154.43 -9.4 9.4 738.59 69.01 150.13 154.43 -9.4 9.4 738.59 69.01 150.13 154.43 -9.4 9.4 9.5 9.4 150.13 154.43 -9.4 9.4 9.5 9.4 9.5 9.4 9.5 9.4 9.5 9.4 9.5 9.5 9.5 9.5 9.5 9.5 9.5 9.5 9.5 9.5	242	740.30	105.32	150.18	154.43	4.0	0.455	634.98	
746.29 87.89 150.01 154.82 -9.4 0.454 159.25 88.25 88.21 150.30 154.42 -9.4 0.455 159.30 154.42 -9.4 0.455 159.30 154.42 -9.4 0.455 159.30 154.42 -9.4 0.455 159.30 154.42 -9.4 0.455 159.30 154.42 -9.4 0.455 159.30 154.43 -9.4 0.455 159.30 154.27 -9.4 0.455 159.31 150.30 154.27 -9.4 0.455 159.31 150.30 154.27 -9.4 0.455 159.31 150.31 154.27 -9.4 0.455 159.31 1738.78 159.31 150.31 154.35 -9.4 0.455 159.31 1738.78 159.04 150.30 154.43 -9.4 0.455 159.30 154.43 -9.4 0.455 159.30 154.43 -9.4 0.455 159.30 154.43 -9.4 0.455 159.30 154.43 -9.4 0.455 159.30 159.30 154.43 -6.3 0.455 159.30 159.30 154.43 -6.3 0.455 159.30 159.30 154.43 -6.3 0.455 159.30 159.30 154.43 -6.3 0.455 159.30 159.30 154.43 -6.3 0.455 159.30 159.30 154.43 -6.3 0.455 159.30 159.30 154.43 -6.3 0.455 159.30 159.30 154.43 -6.3 0.455 159.30 159.30 154.58 -9.4 0.455 159.30 159.30 154.58 -9.4 0.455 159.30 159.30 154.58 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 154.30 -9.4 0.455 159.30 159.30 154.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 159.30 154.30 -9.4 0.455 159.30 15	243 244	740.06	100.87	150.19	154.27	7.00	0.455	645.36	
738.299 85.04 150.30 154.43 -9.4 0.455 739.25 83.31 150.19 154.42 -9.6 0.455 739.25 83.31 150.19 154.42 -9.6 0.455 739.25 83.32 150.30 154.27 -9.4 0.455 739.25 83.03 150.07 154.27 -9.4 0.455 739.25 83.03 150.07 154.27 -9.4 0.455 739.21 74.49 150.01 154.27 -9.4 0.455 739.21 74.49 150.01 154.27 -9.4 0.455 738.78 75 69.01 150.18 154.43 -9.4 0.454 738.78 69.01 150.18 154.43 -9.4 0.454 738.78 70.19 140.83 155.01 154.43 -9.4 0.455 739.04 69.22 150.24 154.43 -9.4 0.455 738.58 69.44 150.07 154.43 -9.4 0.455 738.58 69.44 150.07 154.43 -9.4 0.455 738.58 69.08 149.83 154.43 -9.4 0.455 738.45 69.08 149.95 154.58 -9.4 0.455 738.45 69.08 149.95 154.58 -9.4 0.455 738.45 69.08 149.95 154.58 -9.4 0.455 738.45 69.08 149.95 154.58 -9.4 738.45 69.08 149.95 154.58 -9.4 738.45 66.86 150.07 154.27 -6.3 738.45 66.86 150.13 154.11 -9.4 738.45 66.86 150.13 154.43 -9.4 738.45 66.86 150.13 154.43 -9.4 738.45 66.86 150.13 154.43 -9.4 738.45 66.86 150.13 154.43 -9.4 738.45 66.86 150.13 154.43 -9.4 6.9 738.45 66.86 150.13 154.43 -9.4 6.9 738.45 66.86 150.13 154.43 -9.4 6.9 738.45 66.86 150.13 154.43 -9.4 6.9 738.45 66.86 150.13 154.43 -9.4 6.9 738.45 66.86 150.13 154.43 -9.4 6.9 738.45 66.86 150.13 154.43 -9.4 6.9 738.45 66.86 150.13 154.43 -9.4 6.9 738.45 66.86 150.13 154.43 -9.4 6.9 738.45 66.86 150.13 154.43 -9.4 6.9 738.45 66.86 150.13 154.43 -9.6 738 738.45 66.86 150.13 154.43 -9.4 6.9 738.45 66.86 150.13 154.43 -9.6 738 738.45 66.86 150.13 154.43 -9.6 738 738.45 66.86 150.13 154.43 -9.6 738 738.45 66.86 150.13 154.43 -9.6 738 738 738 738 738 738 738 738 738 738	245	740.29	87.89	150.01	154.82	4.00	0.454	652.40	
739.88 739.88 739.88 739.88 739.88 739.88 739.88 739.67 739.67 739.67 739.67 739.67 739.67 739.67 739.67 739.67 739.67 739.67 738.78 738.78 738.78 738.89	246	739.99	85.04 84.21	150.30	154.43	4.6	0.45 0.45 0.45 0.45	654.95 655.03	
739.56 83.72 150.30 154.27 -9.4 0.455 739.25 82.69 150.07 154.43 -6.3 0.455 739.27 82.69 150.07 154.43 -6.3 0.455 739.21 80.25 150.01 154.21 -9.4 0.455 739.21 80.25 150.01 154.51 -9.4 0.455 739.21 80.25 150.01 154.51 -9.4 0.454 738.78 73 69.01 150.01 154.43 -9.4 0.454 738.96 70.05 149.83 153.88 -6.3 0.455 738.63 69.14 149.83 153.88 -6.3 0.455 738.63 69.01 150.07 154.58 -9.4 0.455 738.63 69.01 150.07 154.58 -9.4 0.455 738.83 69.01 150.07 154.58 -9.4 738.83 69.03 149.83 154.58 -9.4 738.83 69.03 149.83 154.58 -9.4 738.83 69.03 150.13 154.11 -9.4 738.84 68.80 150.13 154.11 -9.4 738.84 68.80 150.13 154.11 -9.4 738.85 68.94 150.13 154.11 -9.4 738.85 69.01 150.13 154.11 -9.4 738.85 69.01 150.13 154.11 -9.4 738.85 68.94 150.13 154.11 -9.4 738.85 68.94 150.13 154.11 -9.4 738.85 69.01 150.13 154.11 -9.4 738.85 69.01 150.13 154.11 -9.4 738.85 69.01 150.13 154.50 -9.4 738.85 69.01 150.13 154.50 -9.4 738.85 69.01 150.13 154.50 -9.4 738.85 69.01 150.13 154.50 -9.4 738.85 69.01 150.13 154.50 -9.4 738.85 69.01 150.13 154.50 -9.4 738.85 69.01 150.13 154.50 -9.4 738.85 69.01 150.13 154.50 -9.4 738.85 69.01 150.01 154.50 -9.4 66.3 -9.4 738.85 69.01 150.01 154.50 -9.4 66.3 -9.4 738.85 69.01 150.01 154.50 -9.4 66.3 -9.4 738.85 69.01 150.01 154.50 -9.4 66.3 -9.4 738.85 69.01 150.01 154.50 -9.4 66.3 -9.4 738.85 69.01 150.01 154.50 -9.4 66.3 -9.4 738.85 69.01 150.01 154.50 -9.4 66.3 -9.4 738.85 69.01 150.01 154.50 -9.4 66.3 -9.4 738.85 69.01 150.01 154.50 -9.4 66.3	. 84 84 84 84 84	739.88	83.31	150.30	154.43	4.6-	0.455	656.57	
739.25 739.27 739.27 739.67 739.67 739.67 739.67 739.67 739.11 74.49 738.78 738.78 738.78 738.89	249	739.56	83.72	150.30	154.27	4.0-	0.455	655.84	
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738.75 738.76 69.84 738.75 738.76 69.84 738.76 69.84 738.96 70.19 150.11 154.19 738.48 70.19 149.95 154.43 -9.4 0.455 738.68 69.22 150.01 154.43 -6.3 0.455 738.68 69.22 150.07 154.58 -9.4 0.455 738.63 69.14 149.83 154.58 -9.4 738.87 69.63 149.95 154.50 -6.3 738.88 69.35 150.07 154.11 -9.4 738.89 68.80 150.13 154.11 -9.4 738.80 68.90 150.13 154.11 -9.4 738.85 68.90 150.13 154.11 -9.4 738.85 68.90 150.13 154.11 -9.4 738.85 68.90 150.13 154.35 -9.4 738.25 68.90 150.10 154.50 -9.4	253	739.11	74.49	150.07	154.35	4.0	0.454	667.13	
738.73 69.01 150.18 154.58 -9.4 0.454 738.96 70.05 149.95 154.42 -9.4 0.455 738.96 70.19 149.83 153.88 -6.3 0.455 738.58 69.22 150.24 154.43 -6.3 738.58 69.914 149.83 154.58 -9.4 738.59 69.10 150.07 154.51 -9.4 738.30 69.70 150.24 154.50 -6.3 738.87 69.63 149.83 154.50 -6.3 738.87 69.63 149.83 154.50 -6.3 738.88 69.35 150.07 154.11 -9.4 738.14 68.80 150.13 154.11 -9.4 738.45 69.01 150.13 154.11 -9.4 738.45 68.86 150.13 154.35 -9.4 738.45 68.86 150.13 154.31 -9.4 738.25 68.86 150.10 154.35 -9.4	255	738.76	69.84	150.19	154.19	4.6-	0.454	668.92	
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738.48 70.19 149.83 153.88 -6.3 738.69 69.22 150.24 154.43 -6.3 738.58 68.94 150.07 154.58 -9.4 738.58 69.01 150.07 154.58 -9.4 738.45 69.01 150.07 154.43 -6.3 738.45 69.63 149.83 154.56 -9.4 738.87 69.63 149.83 154.50 -9.4 738.38 69.35 149.77 154.27 -6.3 738.38 69.35 150.07 154.11 -9.4 738.45 69.01 150.13 154.43 -9.4 738.45 69.01 150.13 154.43 -9.4 738.45 69.01 150.13 154.43 -9.4 738.25 68.86 150.07 154.50 -9.4 738.25 68.86 150.07 154.50 -9.4	25.0	738.96	70.05	149.95	154.43	-6.3	0.455	668.90	
738.69 69.22 150.24 154.43 -6.3 738.58 68.94 150.07 154.58 -9.4 738.63 69.01 150.07 154.43 -6.3 738.30 69.01 150.07 154.43 -9.4 738.45 69.08 150.24 154.58 -9.4 738.87 69.08 149.95 154.58 -9.4 738.53 68.52 149.77 154.27 -6.3 738.38 69.35 150.07 154.11 -9.4 738.14 68.80 150.13 154.11 -9.4 738.45 69.01 150.13 154.43 -9.4 738.25 68.86 150.07 154.35 -6.3	259	738.48	70.19	149.83	153.88	-6.3		668.30	
738.63 69.14 149.83 154.12 -6.3 159.00 69.01 150.07 154.12 -6.3 159.00 69.70 150.07 154.50 -9.4 150.07 154.50 -9.4 150.07 154.50 -9.4 150.07 154.50 -9.4 150.08 149.83 154.50 -9.4 150.08 149.77 154.11 -9.4 150.13 154.11 -9.4 150.13 154.11 -9.4 150.13 154.11 -9.4 150.13 154.11 -9.4 150.13 154.50 -9.4 150.13 154.50 -9.4 150.13 154.50 -9.4 150.18 154.50 -9.4 150.18 154.50 -9.4 150.19 150.19 150.19 150.19 150.19 150.19 150.19 154.50 -9.4 150.19 150.	260	738.69	69.22	150.24	154.43	. o		669.47	
739.00 69.01 150.07 154.43 -9.4 738.30 69.70 150.42 154.50 -6.3 738.87 69.63 149.83 154.50 -6.3 738.53 69.08 149.95 154.58 -9.4 738.53 68.52 149.77 154.51 -9.4 738.80 68.94 150.13 154.11 -9.4 738.45 69.01 150.13 154.11 -9.4 738.25 68.86 150.07 154.35 -9.4 738.25 68.86 150.07 154.50 -9.4	262	738.63	69.14	149.83	154.12	6.3		669.49	
738.30 69.40 150.24 154.50 -9.5 738.87 69.63 149.83 154.58 -9.4 738.53 69.08 149.95 154.58 -9.4 738.53 69.35 149.77 154.11 -9.4 738.80 68.94 150.13 154.11 -9.4 738.45 69.01 150.13 154.43 -9.4 738.25 68.86 150.07 154.66 -9.4 738.25 68.86 150.07 154.50 -9.4	263	739.00	69.01	150.07	154.43	4.6-		669.99	
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738.28 69.08 149.95 154.58 -9.4 738.53 69.35 150.07 154.11 -9.4 738.14 68.80 150.13 154.11 -9.4 738.45 69.01 150.18 154.66 -9.4 738.25 68.86 150.07 154.50 -9.4 738.25 68.86 150.07 154.50 -9.4	266	738.87	69.63	149.83	154.50	-6.3		669.24	
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738.14 68.80 150.13 154.11 -9.4 738.80 68.94 150.13 154.43 -9.4 738.45 69.01 150.18 154.66 -9.4 738.25 68.86 150.19 154.35 -6.3 748.37 68.52 150.07 154.50 -9.4	269	738.38	69.35	150.07	154.11	4.6		669.03	
738.25 68.86 150.19 154.66 -9.4 738.25 68.86 150.19 154.35 -6.3 738.37 68.52 150.07 154.50 -9.4	270 271	738.14	68.80 68.94	150.13	154.11	4.00		669.86	
738.25 68.86 150.19 154.35 -5.3 738.37 68.52 150.07 154.50 -9.4	272	738.45	69.01	150.18	154.66	4.0		669.44	
	273 274	738.25	68.86 58.50	150.19	154.50	0.00		669.85	

Single Brush - position 1 œ CONFIGURATION NO.

	DELTA-P STA 1-5	(DS1D)	66668888888888888888888888888888888888
	AVERAGE LEAKAGE DATE	(LBM/S)	0.000.000.000.000.000.000.000.000.000.
	AVERAGE SHAFT	(RPM)	ݥݟݟݥݟݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥݥ
	AVG TEMP STATION 5	(R)	154.25 154.25 154.25 154.25 155.25 15
- position -	AVG TEMP STATION 1	(R)	149.95 149.89 150.07 150.07 150.09 150.03 15
single Brush	AVG PRESS STATION 5	(PSIA)	69.09.09.09.09.09.09.09.09.09.09.09.09.09
	EN AVG PRESS STATION 1	(PSIA)	737.734 738.737 738.738 738.745 738.745 738.745 737.88.00 737.88.00 737.88.00 737.88.00 755.65 755.65 755.65 777.73.38 777.73.46
CONFIGURALION	FLUID: NITROGEN RDG SCAN		740 227 247 248 248 248 248 248 248 248 248 248 248

DELTA-P STA 1-2 77.88 101.27 101.27 101.27 101.27 101.27 101.27 101.27 102.131 102.131 103.131 (PSID) DELTA-P STA 1-5 77.15 1000.1 (PSID) 2 VENTURI 2 LEAKAGE RATE (LBM/S) 0.0068 0.0026 0.0026 0.0026 0.0027 0. 0.131 0.150 0.163 0.169 6556999 655699 655699 655699 655699 655699 655699 655699 655699 6556999 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 6556999 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 655699 6556999 655699 655699 655699 655699 655699 655699 655699 655699 6556999 655699 655699 655699 655699 655699 655699 655699 655699 6556999 655699 655699 655699 655699 655699 655699 655699 655699 6556999 655699 655699 655699 655699 655699 655699 655699 655699 6556999 655699 655699 655699 655699 655699 655699 655699 655699 6556999 65569 65569 65669 65669 65669 65669 65669 65669 65669 65669 65669 65669 6566 AVERAGE SHAFT SPEED (RPM) ιC AVG TEMP STATION 5 \mathfrak{E} 2 AVG TEMP STATION 2 (R) AVG TEMP STATION 1 48.55 47.74 44.77.74 44.77.79 46.57 3 AVG PRESS STATION 5 353.51 353.51 353.51 331.55 33 AVG PRESS STATION 2 3362.78 2259.72 2255.33 3362.78 3386.33 3386.78 3386.00 3386.33 AVG PRESS STATION 1 440.66
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4 YDROGEN SCANS P NO SOCIO CON CONTRA DE CON FLUID: HYE RDG AVG

FLUID: HYDROGEN

DELTA-P STA 1-2	(PSID)	29.10 25.64 127.86 150.11 127.65 150.12 127.12 127.12 127.13 127.
DELTA-P STA 1-5	(PSID)	28.60 125.10 123.33 126.007 127.003 123.003 123.003 123.003 124.00 124.00 124.00 125.003 125.003 126.003 126.003 127.0
VENTURI 2 LEAKAGE RATE	(LBM/S)	0.077 0.077 0.120 0.152 0.152 0.161 0.148 0.128 0.089 0.094 0.093
AVERAGE SHAFT SPEED	(RPM)	45293.8 35348.8 35340.6 35302.5 35302.5 35302.5 35302.6 35302.
AVG TEMP STATION 5	(R)	85558888888888888888888888888888888888
AVG TEMP STATION 2	(R)	52.33 52.33 52.33 52.33 52.33 52.33 52.33 53.33
AVG TEMP STATION 1	(R)	\$4 699.59 \$4 699.59 \$5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5
AVG PRESS STATION 5	(PSIA)	426.011 369.11 369.11 386.35 386.35 386.35 386.35 386.95 390.20 467.36 467.36 467.36 467.36 391.20 3
AVG PRESS STATION 2	(PSIA)	425.52 425.52 425.52 425.52 425.52 425.52 425.52 425.52 425.52 425.52 425.52 425.52 425.53
N AVG PRESS STATION 1	(PSIA)	440.36 451.11 442.42 432.42 432.62 432.62 443.23 442.53 445.23 445.73 466.85
FLUID: HYDROGEN RDG AVG SCANS A		859 ALL SCNS 861 ALL SCNS 862 ALL SCNS 863 ALL SCNS 864 ALL SCNS 865 ALL SCNS 866 ALL SCNS 866 ALL SCNS 866 ALL SCNS 872 ALL SCNS 873 ALL SCNS 873 ALL SCNS 874 ALL SCNS 882 ALL SCNS 884 ALL SCNS 885 ALL SCNS 886 ALL SCNS 899 A

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13.	ABSTRACT (Maximum 200 words)						

Brush seals are compliant contacting seals and have significantly lower leakage than labyrinth seals in gas turbine applications. Their long life and low leakage make them candidates for use in rocket engine turbopumps. Brush seals, 50.8 mm (2 in.) in diameter with a nominal 127- μ m (0.005-in.) radial interference, were tested in liquid nitrogen (LN₂) and liquid hydrogen (LH₂) at shaft speeds up to 35 000 and 65 000 rpm, respectively, and at pressure drops up to 1.21 MPa (175 psid) per brush. A labyrinth seal was also tested in liquid nitrogen to provide a baseline. The LN₂ leakage rate of a single brush seal with an initial radial shaft interference of 127 μ m (0.005 in.) measured one-half to one-third the leakage rate of a 12-tooth labyrinth seal with a radial clearance of 127 μ m (0.005 in.). Two brushes spaced 7.21 μ m (0.248 in.) apart leaked about one-half as much as a single brush, and two brushes tightly packed together leaked about three-fourths as much as a single brush. The maximum measured groove depth on the Inconel 718 rotor with a surface finish of 0.81 μ m (32 μ in.) was 25 μ m (0.0010-in.) after 4.3 hr of shaft rotation in liquid nitrogen. The Haynes-25 bristles wore approximately 25 to 76 μ m (0.001 to 0.003 in.) under the same conditions. Wear results in liquid hydrogen were significantly different. In liquid hydrogen the rotor did not wear, but the bristle material transferred onto the rotor and the initial 127- μ m (0.005-in.) radial interference was consumed. Relatively high leakage rates were measured in liquid hydrogen. More testing is required to verify the leakage performance, to validate and calibrate analysis techniques, and to determine the wear mechanisms. Performance, staging effects, and preliminary wear results are presented.

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